CDM-MP87-A07

Draft Large-scale Methodology

AM0089: Production of diesel using a mixed feedstock of gasoil and vegetable oil

Version 03.0

Sectoral scope(s): 05, 13 and 15



United Nations Framework Convention on Climate Change

COVER NOTE

1. Procedural background

- 1. The Executive Board of the clean development mechanism (CDM) (hereinafter referred to as the Board), at its 110th meeting, considered the draft revised "Glossary: CDM terms" that contained revised definition of "renewable biomass" and introduced definitions of new terms associated with market penetration of technology/measure, and requested the Methodologies Panel (MP) to analyze the existing approved methodologies and methodological tools with regard to the consistency in the use of these terms and related guidance, and to recommend revision to the methodologies and tools, as appropriate, based on the analysis.
- 2. The Methodologies Panel, at its 86th meeting, proposed a draft revised version of the "TOOL16: Project and leakage emissions from biomass" containing a comprehensive approach to determine emissions from the cultivation of biomass in dedicated plantations, transportation of biomass and biomass residues and treatment of biomass and biomass residues, and launched a call for public inputs. No comments were received.

2. Purpose

3. The purpose is to update this methodology to make consistent reference to the elements from the TOOL16 in the project emissions and leakage sections.

3. Key issues and proposed solutions

- 4. As per the current version of the methodology, project emission due to the use of biomass from dedicated plantations shall be calculated according to the "TOOL16: Project and leakage emissions from biomass". In addition, the methodology requires emissions from the transportation of oil seeds and vegetable oil to be calculated based on the provisions of the "TOOL12: Project and leakage emissions from transportation of freight" and emissions associated with the electricity and fuel consumed and wastewater generated due to the extraction of vegetable oil from the oil seeds in the vegetable oil production plant to be determined, respectively, based on the "TOOL03: Tool to calculate project or leakage CO₂ emissions from fossil fuel combustion", "TOOL05: Baseline, project and/or leakage emissions from electricity consumption and monitoring of electricity generation" and specific equations.
- 5. In the proposed revision, the following project emissions sources are included for projects involving the consumption of biomass, aligned with the proposed revision of the "TOOL16: Project and leakage emissions from biomass":
 - (a) Project emissions resulting from the cultivation of biomass in a dedicated plantation if the biofuel is produced from feedstock that is cultivated in dedicated plantations (e.g. seeds) (PE_{BC});

- (b) Project emissions resulting from the transportation of biomass (e.g. oil seeds) to from the cultivation site to the biomass processing facility (e.g. oil production plant(s)/mill(s)), and from the transportation of biomass (e.g. vegetable oil, waste oil/fats) from the biomass processing facility to the HDS unit (PE_{BT});
- (c) Project emissions resulting from the biomass processing facility (e.g. the oil production plant(s) and/or mill(s)) (PE_{BP}).
- 6. The proposed revision also removes the sections containing the determination of project emissions from the due to the extraction of vegetable oil from the oil seeds in the vegetable oil production plant ($PE_{VOP,y}$) and project emissions from the transportation of oil seeds and vegetable oil ($PE_{TR,y}$) and the monitoring of relevant parameters since these sources are already quoted in the proposed revision of the "TOOL16: Project and leakage emissions from biomass".

4. Impacts

7. The revision of this methodology, along with the revision of the "TOOL16: Project and leakage emissions from biomass", if approved, will provide clarity to stakeholders on the emission sources that may need to be included in the calculation of project emissions from projects involving the use of biomass or biomass residues.

5. Subsequent work and timelines

8. The MP, at its 87th meeting, agreed to seek public inputs on the draft revised methodology. Inputs received, if any, will be discussed with the MP and forwarded to the Board for its consideration together with this document. No further work is envisaged.

6. Recommendations to the Board

9. The MP recommends that the Board adopt this draft methodology, to be made effective at the time of the Board's approval.

TABLE OF CONTENTS

Page

| 1. | INTRO | | Ν | 6 | | | | |
|----|--|--|--|----|--|--|--|--|
| 2. | SCOPE, APPLICABILITY, AND ENTRY INTO FORCE | | | | | | | |
| | 2.1. | Scope | | | | | | |
| | 2.2. | Applicat | pility | 6 | | | | |
| | 2.3. | Entry int | o force | 7 | | | | |
| 3. | NORMATIVE REFERENCES | | | | | | | |
| | 3.1. | Selected approach from paragraph 48 of the CDM modalities and procedures | | | | | | |
| | 3.2. | Applicat | pility of sectoral scopes | 8 | | | | |
| 4. | DEFIN | NITIONS | | 8 | | | | |
| 5. | BASELINE METHODOLOGY | | | | | | | |
| | 5.1. | Project boundary | | | | | | |
| | 5.2. | Selection of the baseline scenario and demonstration of additionality | | | | | | |
| | | 5.2.1. | Step 1.1: Identify all realistic and credible alternatives for the production of diesel | 12 | | | | |
| | | 5.2.2. | Step 1.2: Eliminate alternatives that are not complying with applicable laws and regulations | 13 | | | | |
| | | 5.2.3. | Step 1.3: Compare economic attractiveness of remaining alternatives | 13 | | | | |
| | | 5.2.4. | Step 2.1: Identify all realistic and credible alternatives for the land use | 13 | | | | |
| | | 5.2.5. | Step 2.2: Eliminate alternatives that are not complying with applicable laws and regulations | 13 | | | | |
| | | 5.2.6. | Step 2.3: Eliminate alternatives that face prohibitive barriers | 13 | | | | |
| | | 5.2.7. | Step 2.4: Compare economic attractiveness of remaining alternatives | 14 | | | | |
| | 5.3. | Addition | Additionality | | | | | |
| | | 5.3.1. | Guidance for the Barriers Analysis when the dedicated plantation (or part of) is covered under an A/R CDM project activity | 14 | | | | |
| | 5.4. | Fmissio | n reductions | 15 | | | | |
| | 5.5. | | e emissions | 15 | | | | |

| APPE | ENDIX 2 | . CLIMA | TE ZONE | 37 |
|------|---------|------------|--|----|
| APPE | ENDIX 1 | | RMINATION OF FACTOR F IN THE PRODUCTION OF OGEN | 35 |
| | 6.1. | Data and | parameters monitored | 29 |
| 6. | MONIT | | ETHODOLOGY | 28 |
| | 5.8. | Data and | parameters not monitored | 23 |
| | | 5.7.2. | Determination of Q _{RD, y} | 23 |
| | | 5.7.1. | Determination of <i>Q_{NG,Es,y}</i> | 22 |
| | 5.7. | Leakage | | 19 |
| | | 5.6.2. | Determination of <i>PE_{H2,y}</i> | 17 |
| | | 5.6.1. | Determination of <i>PE_{Biomass,y}</i> | 16 |
| | 5.6. | Project en | nissions | 15 |
| | | | | |

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1. Introduction

1. The following table describes the key elements of the methodology:

| Table 1. | Methodology key elements | |
|----------|--------------------------|--|
|----------|--------------------------|--|

| Typical project(s) | Production of petro/renewable diesel by switching the feedstock of hydrodesulphurization process (HDS) unit from 100 % gasoil to a mixture of gasoil and vegetable oil in an existing refinery, where the vegetable oil comes from oilseeds from plants that are cultivated on dedicated plantations established on lands that are degraded or degrading at the start of the project | | |
|--|--|--|--|
| Type of GHG emissions mitigation action | Renewable energy; Feedstock switch. Displacement of more-GHG-intensive feedstock for the production of diesel | | |

2. Scope, applicability, and entry into force

2.1. Scope

2. This methodology applies to project activities that produce petro/renewable diesel, by switching the feedstock from 100% gasoil to a mixture of gasoil and vegetable oil in an existing refinery.

2.2. Applicability

- 3. The methodology is applicable under the following conditions:
 - (a) Production of petro/renewable diesel:
 - (i) The project activity is carried out in a refinery that was producing only petrodiesel and no renewable diesel during the last three years prior to the start of the project activity. Under the project activity, the feedstock of the hydrodesulphurization process (HDS) unit is changed from 100 % gasoil to a mixture of gasoil and vegetable oil in the production of diesel. In case the project activity is introduced in new HDS unit, the project participants must have historical data of three years prior to the implementation of CDM project activity related to the petrodiesel produced by the refinery and the existing HDS unit;
 - (ii) The energy consumption in the HDS unit under the project activity is lower or equal to the baseline scenario;

- (iii) Natural gas¹ is used as feedstock and fuel to produce hydrogen (H₂) in both the baseline scenario and under the project activity;
- (iv) Under the project activity, any combustible gases and off-gases formed during the hydrogenation of vegetable oil are flared and/or used in the refinery as fuel.
- (b) Consumption of petro/renewable diesel:
 - (i) The petro/renewable diesel produced under the project activity is not exported to the Annex I country;
 - (ii) Only petro/renewable diesel consumed in excess of mandatory regulations is eligible for the purpose of the project activity.²
- 4. In addition, the applicability conditions included in the tools referred to below shall apply.
- 5. Finally, the methodology is only applicable if the most plausible baseline scenario, as identified per the section "Selection of the baseline scenario and demonstration of additionality" hereunder, is:
 - (a) For production of diesel (P): scenario P1; and
 - (b) For land used for plantations (L): scenario L1.

2.3. Entry into force

6. The date of entry into force is the date of the publication of the EB xx meeting report on DD Month 2022.

3. Normative references

- 7. This baseline and monitoring methodology is based on the following approved baseline and monitoring methodologies and proposed new methodologies:
 - (a) ACM0017 "Production of biodiesel for use as fuel" (hereinafter referred as ACM0017);
 - (b) NM0312 "Production of diesel using a mixed feedstock of gasoil and vegetable oil at the inlet of Hydrotreatment Units" prepared by Alberto Pasqualini REFAP S.A.
- 8. This methodology also refers to the latest approved versions of the following tools:
 - (a) **"TOOL01:** Tool for the demonstration and assessment of additionality" (hereinafter referred as TOOL01);

¹ The project participants can request for the revision of this methodology if they use different types of fuel in project scenario than baseline scenario and use other types of fuel than natural gas.

² Regulations that have been implemented since the adoption by the COP of the CDM M&P (decision 17/CP.7, 11 November 2001) need not be taken into account.

- (b) <u>"TOOL05:Tool to calculate baselineBaselineBaseline"</u>, project and/or leakage emissions from electricity consumption and monitoring of electricity generation" (hereinafter referred as TOOL05);
- (c) "TOOL07: Tool to calculate emission factor for an electricity system" (hereinafter referred as TOOL07);
- (d) **"TOOL03:** Tool to calculate project or leakage CO₂ emissions from fossil fuel combustion" (hereinafter referred as TOOL03);
- (e) **"TOOL06:** Project emissions from flaring" (hereinafter referred as TOOL06);
- (f) Project and leakage emissions from transportation of freight;
- (g) <u>"TOOL15:</u> Upstream leakage emissions associated with fossil fuel use" (hereinafter referred as TOOL15);
- 9. Assessment of the validity of the original/current baseline and update of the baseline at the renewal of the crediting period.
- 10. For more information regarding the proposed new methodologies and the tools as well as their consideration by the Executive Board please refer to < http://cdm.unfccc.int/methodologies/PAmethodologies/approved >.

3.1. Selected approach from paragraph 48 of the CDM modalities and procedures

11. "Existing actual or historical emissions, as applicable".

3.2. Applicability of sectoral scopes

- 12. For validation and verification of CDM projects and programme of activities by a designated operational entity (DOE) using this methodology, the following sectoral scopes are mandatory:
 - (a) If biofuel is produced from biomass residues as a feedstock for:
 - (i) Stationary applications, then sectoral scope 5 and 1 apply;
 - (ii) Transportation, then sectoral scopes 5 and 7 apply.
 - (b) If biofuel is produced from anything other than biomass residues as a feedstock for:
 - (i) Stationary applications, then sectoral scopes 1, 5, 1 and 15 apply;
 - (ii) Transportation, then sectoral scopes 5, 7 and 15 apply.

4. Definitions

13. The definitions contained in the Glossary of CDM terms shall apply.

- 14. For the purpose of this methodology, the following definitions apply:
 - (a) **Biogenic** means that the oils and/or fats originate from either vegetable or animal biomass, but not from mineral (fossil) sources;
 - (b) **Dedicated plantations** plantations that are newly established as part of the project activity for the purpose of supplying oils seeds to project activity;
 - (c) **Degraded or degrading lands** lands that can be identified as degraded or degrading as per the "Tool for the identification of degraded or degrading lands for consideration in implementing CDM A/R project activities";
 - (d) **Refinery** a plant which produces petrodiesel and/or renewable diesel from gasoil or vegetable oil;
 - (e) **Existing refinery** a refinery which started commercial operation at least three years prior to the start of the CDM project activity;
 - (f) **Gasoil** a mixture of middle distillates from various refinery streams for example: heavy and light atmospheric distillate and fluid catalytic cracking middle distillate (light cycle oil or coking gasoil) that constitute the feedstock for the hydrodesulphurization (HDS) unit;
 - (g) Hydrodesulphurization process (HDS) the process that consists of the addition of hydrogen to gasoil at high pressure and high temperature using a catalyst. This process, traditionally used in oil refineries for removal of sulphur, nitrogen, olefins and aromatic compounds from gasoil by means of several kinds of reactions, is also suitable for carrying out vegetable oil hydrogenation;
 - (h) **Petrodiesel** diesel produced only from petroleum sources, such as gasoil;
 - (i) **Petrodiesel HS** petrodiesel with high sulphur content;
 - (j) **Petrodiesel LS** petrodiesel with low sulphur content;
 - (k) Petro/renewable diesel the mixture of petrodiesel and renewable diesel and is produced through the hydrogenation of vegetable oil along with gasoil carried out in operating oil refineries, and with the same technical specification, according to national norms and regulations, to the diesel oil;
 - (I) **Renewable diesel** fuel produced through hydrogenation of vegetable oil;
 - (m) **Vegetable oil** oil of biogenic origin that is produced from oil seeds from plants.

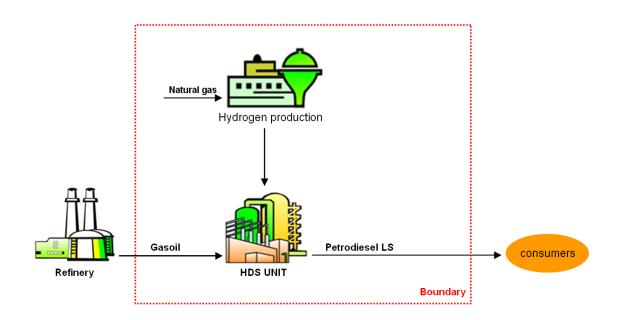
5. Baseline methodology

5.1. Project boundary

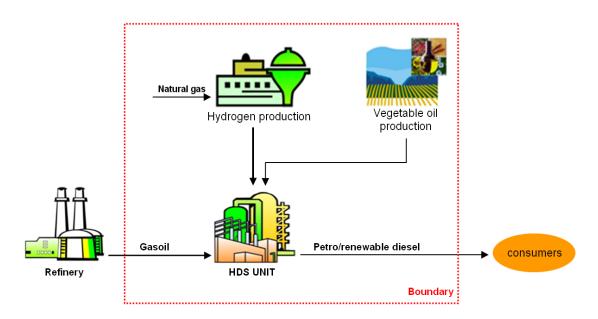
- 15. The **spatial extent** of the project boundary encompasses:
 - (a) The HDS plant;
 - (b) The hydrogen production plant;

- (c) The vegetable oil production plant(s);
- (d) The dedicated plantations.
- 16. Simplified diagrams of the baseline scenario and project activity are presented in Figures 1 and 2.

Figure 1. Baseline Scenario







CDM-MP87-A07 Draft Large-scale Methodology: AM0089: Production of diesel using a mixed feedstock of gasoil and vegetable oil Version 03.0 Sectoral scope(s): 05, 13 and 15

DRAFT

17. The greenhouse gases included in or excluded from the project boundary are shown in Table 2.

| | Source | Gas | Included | Justification/Explanation |
|------------------|--|------------------|----------|---|
| | | CO ₂ | Yes | Main emission source |
| Baseline | Consumption of petrodiesel | CH ₄ | No | Excluded for simplification. This is conservative |
| Ba | poliodicoci | N ₂ O | No | Excluded for simplification. This is conservative |
| | Durchustian of success | CO ₂ | Yes | Main emission source |
| | Production of excess hydrogen (H ₂) | CH ₄ | No | Excluded for simplification |
| | | N ₂ O | No | Excluded for simplification |
| | T | CO ₂ | Yes | Main emission source |
| | Transportation of oil seeds and vegetable oil | CH ₄ | No | Excluded for simplification |
| Ϊţ | | N_2O | No | Excluded for simplification |
| Project activity | Energy consumption for | CO ₂ | Yes | Main emission source |
| tac | production of vegetable | CH ₄ | No | Excluded for simplification |
| jec | oil | N ₂ O | No | Excluded for simplification |
| Pro | Anaerobic treatment of | CO ₂ | No | Excluded for simplification |
| | wastewater from the | CH ₄ | Yes | Main emission source |
| | production of vegetable oil | N ₂ O | No | Excluded for simplification |
| | Cultivation of land to | CO ₂ | Yes | Main emission source |
| | produce oil seeds in | CH ₄ | Yes | Main emission source |
| | dedicated plantations | N ₂ O | Yes | Main emission source |

 Table 2.
 Emission sources included in or excluded from the project boundary

5.2. Selection of the baseline scenario and demonstration of additionality

- 18. The baseline scenario should be separately determined for the following elements:
 - (a) Production of diesel (P); and
 - (b) Land used for plantations (L).
- 19. For the **production of diesel (P)**, the baseline scenario should be determined as follows:

5.2.1. Step 1.1: Identify all realistic and credible alternatives for the production of diesel

- 20. Project participants should at least consider the following alternatives with respect to the production of diesel, inter alia:
 - (a) P1: Production of diesel from 100% gasoil in the existing refinery and the existing HDS unit;
 - (b) P2: Production of diesel from different mix of vegetable oil and gasoil than project activity;

(c) P3: The proposed project activity not undertaken as a CDM project activity.

5.2.2. Step 1.2: Eliminate alternatives that are not complying with applicable laws and regulations

21. Eliminate alternatives that are not in compliance with all applicable legal and regulatory requirements. Apply Sub-step 1b of the latest version of the "Tool for the demonstration and assessment of additionality".

5.2.3. Step 1.3: Compare economic attractiveness of remaining alternatives

- 22. Compare the economic attractiveness for all the remaining alternatives by applying Step 2 of the latest version of the "Tool for the demonstration and assessment of additionality". Provide all the assumptions in the CDM-PDD.
- 23. Include a sensitivity analysis applying Sub-step 2d of the latest version of the "Tool for the demonstration and assessment of additionality". If the sensitivity analysis is conclusive (for a realistic range of assumptions), then the most cost effective scenario is the baseline scenario. In case the sensitivity analysis is not fully conclusive, select the baseline scenario alternative with least emissions among the alternatives that are the most economically attractive according to the investment analysis and the sensitivity analysis.
- 24. For the **land use where the dedicated plantations are established (L)**, the baseline scenario should be determined as follows:

5.2.4. Step 2.1: Identify all realistic and credible alternatives for the land use

- 25. Project participants should at least consider the following alternatives with respect to the baseline scenario for the use of the land where the dedicated plantations are established, inter alia:
 - (a) L1: Continuation of current land use;
 - (b) L2: Conversion to another plantation (annual or perennial);
 - (c) L3: Conversion to oil plant plantations without CDM.

5.2.5. Step 2.2: Eliminate alternatives that are not complying with applicable laws and regulations

26. Eliminate alternatives that are not in compliance with all applicable legal and regulatory requirements. Apply Sub-step 1b of the latest version of the "Tool for the demonstration and assessment of additionality".

5.2.6. Step 2.3: Eliminate alternatives that face prohibitive barriers

27. Scenarios that face prohibitive barriers (e.g. technical barrier) should be eliminated by applying Step 3 of the latest version of the "Tool for the demonstration and assessment of additionality".

5.2.7. Step 2.4: Compare economic attractiveness of remaining alternatives

- 28. Compare the economic attractiveness for all the remaining alternatives by applying Step 2 of the latest version of the "Tool for the demonstration and assessment of additionality". Provide all the assumptions in the CDM-PDD.
- 29. Include a sensitivity analysis applying Sub-step 2d of the latest version of the "Tool for the demonstration and assessment of additionality". If the sensitivity analysis is conclusive (for a realistic range of assumptions), then the most cost effective scenario is the baseline scenario. In case the sensitivity analysis is not fully conclusive, select the baseline scenario alternative with least emissions among the alternatives that are the most economically attractive according to the investment analysis and the sensitivity analysis.
- 30. The project participants should demonstrate that the most plausible scenario is the "continuation of current land use (L1)", by assessing the attractiveness of the plausible alternative land uses in terms of benefits to the project participants, consulting with stakeholders for existing and future land use, and identifying barriers for alternative land uses. This can be done by demonstrating that similar lands in the vicinity are not planned to be used for alternative land uses other than L1. Show that apparent financial and/or other barriers, which prevent alternative land uses can be identified.

5.3. Additionality

- 31. The additionality of the project activity shall be demonstrated and assessed using the latest version of the "Tool for the demonstration and assessment of additionality".
- 32. Where Step 2 of the "Tool for the demonstration and assessment of additionality" (Investment Analysis) is used, the investment analysis shall include a sensitivity analysis of the petro/renewable diesel sales price, the feedstock costs and fuel costs.

5.3.1. Guidance for the Barriers Analysis when the dedicated plantation (or part of) is covered under an A/R CDM project activity

- 33. If the A/R CDM activity and the activity covering the production, sale and consumption of petro/renewable diesel are two independent project activities (which may imply also that project proponents are different) then:
 - (a) A barrier related to the implementation of the plantation cannot be used for the project activity covering the production, sale and consumption of petro/renewable diesel;
- 34. If the A/R CDM project activity and the project activity covering the production, sale and consumption of petro/renewable diesel are part of an integrated development project (which means that the same project proponents are to be involved in the two CDM activities) then:
 - (a) A barrier related to the implementation of the plantation can also be used by the production, sale and consumption of petro/renewable diesel.
- 35. Investment in the establishment of dedicated plantations must be considered, whether or not the establishment of such plantations is part of an A/R CDM project activity, if there is no market for the oil seeds. By definition, tCERs from A/R CDM activities, whose

plantations are part of the project activity, implemented under this methodology and CERs accruing from CDM project activities under this methodology must not be included in the investment analysis performed in order to identify the baseline scenario.

5.4. Emission reductions

36. Emission reductions are calculated as follows:

$$ER_y = BE_y - PE_y - LE_y$$
 Equation (1)

Where:

| ER_y | = | Emission reductions in year y (tCO ₂) |
|--------|---|---|
| BE_y | = | Baseline emissions in year y (tCO ₂) |
| PEy | = | Project emissions in year y (tCO ₂) |
| LE_y | = | Leakage emissions in year y (tCO ₂) |

5.5. Baseline emissions

37. Baseline emissions include the emissions associated with the consumption of petrodiesel by the consumers which is displaced by the use of renewable diesel. The baseline emissions are calculated as follows:

$$BE_{y} = Q_{VO,y} \times R_{RD} \times d_{RD} \times NCV_{PD,y} \times EF_{CO2,PD} \times 10^{-6}$$
 Equation (2)

Where:

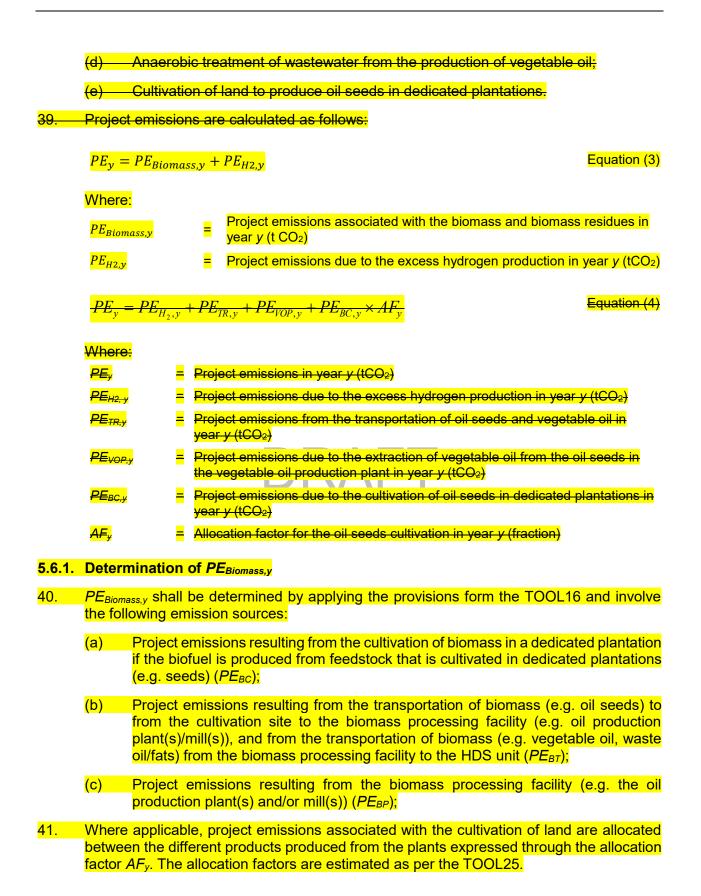
| BE_y | Baseline emissions in year y (tCO₂) |
|-----------------------------|--|
| $Q_{VO,y}$ | = Amount of vegetable oil fed to HDS unit in year y (m ³) |
| R _{RD} | Ratio between the amount of renewable diesel produced per vegetable oil fed into the HDS unit (m³ renewable diesel / m³ vegetable oil) |
| $d_{\scriptscriptstyle RD}$ | Density of renewable diesel (tonne/m³) |
| $NCV_{PD,y}$ | Average net calorific value of petrodiesel in year y (MJ/tonne) |
| EF _{CO2,PD} | = CO ₂ emission factor of petrodiesel (tCO ₂ /TJ) |

5.6. Project emissions

- 38. Project emissions include emissions from the following sources are calculated as follows:
 - (a) Production of excess hydrogen (H2) that is required in the project scenario to be used in the HDS unit in comparison to the baseline scenario;

(b) Transportation of oil seeds and vegetable oil;

(c) Energy consumption for the production of vegetable oil;



| PE _{Biomass,y} | $= PE_{BP,y}$ | $(+PE_{BT,y} + (AF_y \times PE_{BC,y}))$ Equation (5) |
|-------------------------|---------------|--|
| Where: | | |
| $PE_{BP,y}$ | = | Project emissions resulting from the biomass processing facility and from the biodiesel production plant (tCO ₂ e) |
| PE _{BT,y} | = | Project emissions resulting from the transportation of biomass from the cultivation site to the biomass processing facility, and from the biomass processing facility to the biodiesel production plant (tCO ₂ e) |
| PE _{BC,y} | = | Project emissions resulting from the cultivation of biomass in a dedicated plantation (tCO ₂ e) |
| Droject part | icinante i | may alternatively choose a simplified approach to calculate PE- |

42. Project participants may alternatively choose a simplified approach to calculate $PE_{BC,y}$ using conservative **default values** for the emissions associated with the cultivation of lands. This approach can only be used for **palm or jatropha** based on the equation below:

$$PE_{BC,y} = \sum_{s} A_{s,y} \times EF_{s,y}$$

Where:

| PE _{BC,y} | = | Project emissions associated with the cultivation of land to produce biomass feedstock in year <i>y</i> (tCO ₂) |
|--------------------|---|---|
| $A_{s,y}$ | = | Area in which feedstock type <i>s</i> is cultivated for use in the project plant in year <i>y</i> (ha) |
| EF _{s,y} | = | Default emission factor for the GHG emissions associated with the cultivation of land to produce feedstock type <i>s</i> (tCO ₂ e/ha). See Table 3 below for available values. |

Equation (6)

 Table 3.
 Conservative default emission factors for the GHG emissions associated with

 the cultivation of land to produce biomass feedstock

| Feedstock type s | Tropical Moist ³ | Tropical Wet ³ |
|------------------|-----------------------------|---------------------------------------|
| Palm | <mark>1.87 tCO₂e/ha</mark> | <mark>1.87 tCO₂e/ha</mark> |
| Jatropha | <mark>1.76 tCO₂e/ha</mark> | <mark>2.52 tCO₂e/ha</mark> |

5.6.2. Project emissions due to the excess hydrogen production Determination of PE_{H2,y}

- 43. The project emission due to the excess hydrogen production shall include:
 - (a) The emissions due to the fossil fuel (in this case natural gas) combusted to produce excess hydrogen required to process vegetable oil in the HDS unit;

³ See Appendix 2

- (b) The emissions due to the chemical reaction that forms the excess hydrogen required to process vegetable oil in the HDS unit.
- 44. The project emission due to the excess hydrogen production shall be calculated as follows:

$$PE_{H2,y} = PE_{NG,H2,y} + PE_{CO2,H2,y}$$

Equation (7)

Where:

| PE _{H2,y} | = Project emissions due to the excess hydrogen production in year y (tCO ₂) |
|------------------------------|---|
| PE _{NG,H2,y} | Project emissions due to natural gas combusted to produce excess hydrogen required to process vegetable oil in the HDS unit in year y (tCO₂) |
| <i>РЕ_{СО2,H2,y}</i> | Project emissions due to the chemical reaction that forms the excess hydrogen required to process vegetable oil in the HDS unit in year y (tCO₂) |

5.6.2.1. **Determination of PE_{NG,H2,y}**

45. Project emissions due to natural gas combusted to produce excess hydrogen required to process vegetable oil in the HDS unit shall be calculated as follows:

$$PE_{NG,H2,y} = VR_{H2,ES,y} \times r_{E,H2} \times EF_{CO2,NG} \times 10^{-6}$$
 Equation (8)

Where:

| Where: | | |
|-----------------------|---|---|
| PE _{NG,H2,y} | = | Project emissions due to natural gas combusted to produce H_2 required by the HDS unit during the year <i>y</i> (tCO ₂) |
| $VR_{H2,Es,y}$ | = | Volume of excess H_2 required in the HDS unit in year y (Nm ³ H ₂) |
| $r_{E,H2}$ | = | Rate of energy consumption for H_2 production (MJ/Nm ³ H ₂) |
| EF _{CO2,NG} | = | CO_2 emission factor of natural gas consumed (tCO ₂ /TJ) |
| | | |

5.6.2.2. Determination of VR_{H2,Es,y}

$$VR_{H2,ES,y} = VC_{H2,y} - \left[Q_{PRD,y} \times \frac{\sum_{x=1}^{3} VC_{H2,x}}{\sum_{x=1}^{3} Q_{PD,x}}\right]$$
 Equation (9)

Where:

| VR _{H2,Es,y} | = | Volume of excess H_2 required in the HDS unit in year y (Nm ³ H ₂) |
|-----------------------|---|---|
| VC _{H2,y} | = | Volume of H_2 consumed in the HDS unit in the year y (Nm ³ H ₂) |
| Q _{PRD,y} | = | Total amount of petro/renewable diesel produced by the project activity in year y (m ³) |
| $VC_{H2,x}$ | = | Volume of H_2 consumed in the HDS unit in year x (Nm ³ H ₂) |
| $Q_{PD,x}$ | = | Amount of petrodiesel produced in year x (m ³) |
| x | = | The most recent three years prior to the implementation of the project activity |

5.6.2.3. Determination of $r_{E,H2}$

$$r_{E,H2} = \frac{\sum_{x=1}^{3} FC_{NG,H2,x} \times NCV_{NG,x}}{\sum_{x=1}^{3} VP_{H2,x}}$$
 Equation (10)

Where:

| r _{E,H2} | Rate of energy consumption for H₂ production (MJ/Nm³ H₂) |
|--------------------------|---|
| FC _{NG,H2,x} | = Amount of natural gas consumed as fuel for H_2 production in year x (Nm ³) |
| NCV _{NG,x} | Net calorific value of natural gas combusted in year x (MJ/Nm³) |
| $VP_{H2,x}$ | = Volume of H_2 produced in the H_2 production facility in year x (Nm ³ H ₂) |
| x | = The most recent three years prior to the implementation of the project activity |

5.6.2.4. Determination of *PE*_{CO2,H2,y}

46. Project emissions due to the chemical reaction that forms the excess hydrogen required to process vegetable oil in the HDS unit shall be determined as follows:

$$PE_{CO_2,H_2,y} = F \times VR_{H_2,ES,y} \times 10^{-6}$$
Equation (11)
With
$$F = 490.6 \times \eta_{H_2,react,y}$$
Equation (12)

Where:

| РЕ_{СО2, Н2, у} | Project emissions due to the chemical reaction that forms the excess hydrogen required to process vegetable oil in the HDS unit in year y (tCO₂) |
|--------------------------------|--|
| F | Factor used to relate the volume of H₂ produced to the mass of CO₂ emitted in the reaction (gCO₂/Nm³ H₂), refer to Appendix 2 |
| $VR_{H2,Es,y}$ | = Volume of excess H_2 required in the HDS unit in year y ($Nm^3 H_2$) |
| $\eta_{H2,react,y}$ | Reaction efficiency of H₂ formation in year y |

5.6.3. Project emissions from the transportation of oil seeds and vegetable oil

- 47. Project emissions from transportation of oil seeds and vegetable oil only have to be accounted if distances of more than 50 km are covered.
- 48. Project emissions from transportation oil seeds and vegetable oil include the following sources, where applicable:

(a) Any transportation of oil seeds to the vegetable oil production plant(s);

(b) Any transportation of vegetable oil to the HDS unit.

49. Project emissions from transportation oil seeds and vegetable oil are determined using the latest version of the tool "Project and leakage emissions from transportation of freight". PETR,m in the tool corresponds to the parameter PETR,y in this methodology and the monitoring period m is one year.

5.6.4. Project emissions due to the extraction of vegetable oil from the oil seeds in the vegetable oil production plant

- 50. The project emission due to the extraction of vegetable oil from the oil seeds in the vegetable oil production plant shall include:
 - (a) The emissions due to the energy consumption (fossil fuel and/or electricity) for the production of vegetable oil; and
 - (b) The emissions due to the anaerobic treatment of wastewater from the production of vegetable oil.

| PF | = PE | $\perp PF$ | $\perp PF$ | |
|---------------|-----------------|------------|--------------|------------|
| $I L_{VOP,y}$ | $, -I L_{FC,J}$ | v L EC | y L_{WW} | , <i>у</i> |

Equation (13)

Where:

| PE _{VOP,y} | = | Project emissions due to the extraction of vegetable oil from the oil seeds in the vegetable oil production plant, including transportation in year y (tCO ₂) |
|---------------------------|---|---|
| PE _{FC, y} | = | Project emissions from fossil fuel combustion by the project activity in year y (tCO₂) |
| PE _{EC,y} | = | Project emissions from electricity consumption by the project activity in year y (tCO ₂) |
| P <u>E_{WW,y}</u> | = | Project emissions from anaerobic treatment of wastewater from the vegetable oil production plant in year y (tCO ₂) |

5.6.4.1. Determination of PE_{FC,y}

51. Project emissions from fossil fuel combustion by the project activity in year y (PE_{FC,y}) are calculated using the latest approved version of the "Tool to calculate project or leakage CO₂ emissions from fossil fuel combustion", where the sources j in the tool correspond to all sources of fossil fuel consumption by the project activity, including vegetable oil production plant(s). Fossil fuel consumption, if any, for electricity generation should not be included. All emission sources should be documented transparently in the CDM-PDD.

5.6.4.2. Determination of PE_{EC,y}

52. Project emissions from electricity consumption by the project activity in year y (PE_{EC,y}) are calculated using the latest version of the "Tool to calculate baseline, project and/or leakage emissions from electricity consumption" where the electricity consumption sources j in the tool corresponds to all electricity consumption sources under the project activity, including the vegetable oil production plant. All emission sources should be documented transparently in the CDM PDD.

5.6.4.3. Determination of PE_{WW,y}

5.6.4.3.1. In case that the methane from the anaerobic treatment of wastewater is vented to the atmosphere:

53. If the methane from anaerobic treatment of wastewater is vented to the atmosphere, the project emissions from anaerobic treatment of wastewater from the vegetable oil production plant (*PE_{ww,y}*) are calculated as follows:

$$\frac{PE_{WW,y}}{PE_{WW,y}} = \sum_{d=1}^{365} Q_{WW,d,y} \times COD_{WW,d,y} \times B_0 \times MCF_P \times GWP_{CH4}$$

Where:

| ₽E _{₩₩,y} | = | Project emissions from anaerobic treatment of wastewater from the vegetable oil production plant in year <i>y</i> (tCO ₂) |
|---------------------------------|---|--|
| <mark>Q_{₩₩,d,y}</mark> | = | Amount of wastewater treated anaerobically or released untreated from the vegetable oil production plant on day <i>d</i> in year y (m³) |
| COD _{WW,d,y} | = | Chemical Oxygen Demand (COD) of wastewater on day <i>d</i> in year y (tCOD/m ³) |
| <mark>₿₀</mark> | _ | Maximum methane producing capacity (tCH₄/tCOD) |
| MCF _p | _ | Methane conversion factor (fraction) |
| GWP _{CH4} | = | Global warming potential of methane (tCO ₂ /tCH ₄) |

5.6.4.3.2. In case that the methane from the anaerobic treatment of wastewater is flared:

54. If the methane from anaerobic treatment of wastewater is flared, then the "Tool to determine project emissions from flaring gases containing methane" should be used to estimate project emissions from anaerobic treatment of wastewater from the vegetable oil production plant (*PE*_{WW,y}).

5.6.4.4. Project emissions from the cultivation of oil seeds in dedicated plantations

- 55. Project emissions from the cultivation of oil seeds in dedicated plantations are calculated using one of the following two options:
 - (a) Option 1: This option follows the latest version of the tool "Project emissions from cultivation of biomass";
 - (b) Option 2: This option can only be used for oil seeds from palm or jatropha. In this option a simple approach is apply, using conservative default values for the emissions associated with the cultivation of lands, taking into account different geographical regions.

5.6.4.4.1. Option 1: Tool for Project emissions from cultivation of biomass

56. In this option, PE_{BC,y} in this methodology corresponds to the PE_{BC,y} in the Tool.

5.6.4.4.2. Option 2: Use of a default emission factor

$$PE_{BC,y} = \sum_{s} A_{s,y} \times EF_{s,y}$$
Equation (15)Where: $PE_{BC,y}$ $=$ $PE_{BC,y}$ $=$ $Project emissions from the cultivation of oil seeds in dedicated plantations in year y (tCO2) $A_{s,y}$ $=$ $Area in which oil seed type s is cultivated for use in the project plant in year y (ha) $EF_{s,y}$ $=$ $Default emission factor for the GHG emissions associated with the cultivation of land to produce oil seed type s (tCO2/ha). See below for available values$$$

Table 4. Conservative default emission factors for the GHG emissions associated with the cultivation of land to produce oil seeds during one year

| Crop | <mark>Climate Zone⁴</mark> | <mark>EF_{s,y} (tCO₂e/ha)</mark> |
|-----------------------|-----------------------------|--|
| <mark>Palm</mark> | Tropical Moist | <mark>1.87</mark> |
| <mark>Palm</mark> | Tropical Wet | <mark>1.87</mark> |
| <mark>Jatropha</mark> | <mark>Tropical Moist</mark> | <mark>1.76</mark> |
| Jatropha | <mark>Tropical Dry</mark> | <mark>2.52</mark> |
| . L | | |

5.7. Leakage

- 57. Leakage emissions (LE_y) include the upstream emissions of excess natural gas required for the production of hydrogen and the positive leakage associated with the avoided production of petrodiesel.
- 58. Leakage emissions in year y (LE_y) shall be determined using the latest version of the TOOL15methodological tool "Upstream leakage emissions associated with fossil fuel use" where $LE_{US,y}$ refers to LE_y , $FC_{PJ,x,y}$ refers to $Q_{NG,Es,y}$ and $FC_{BL,x,y}$ refers to $Q_{RD,y}$ in this methodology.
- 59. Where total net leakage effects from upstream emissions are negative ($LE_y < 0$), project participants should assume $LE_y = 0$.

5.7.1. Determination of Q_{NG,Es,y}

$$Q_{NG,ES,y} = VR_{H_2,ES,y} \times \frac{\sum_{1}^{3} (Q_{NG,FS,x} + FC_{NG,H_2,x})}{\sum_{1}^{3} VP_{H_2,x}}$$
Equation (16)

Where:

Q_{NG,Es,y}

 Amount of excess of natural gas used as feedstock and fuel for H₂ production between baseline scenario and project activity in year y (Nm³)

⁴ See Appendix 3.

| VR _{H2,Es,y} | Volume of excess H ₂ required in the HDS unit in year y (Nm ³ H ₂) (Calculated following the equation 6 above.) |
|-----------------------|---|
| Q _{NG,FS,x} | Amount of natural gas used as feedstock for H_2 production in year x (Nm ³) |
| FC _{NG,H2,x} | Amount of natural gas consumed as fuel for H_2 production in year x (Nm ³) |
| $VP_{H2,x}$ | Volume of H_2 produced in the H_2 production facility in year x (Nm ³ H ₂) |
| x | The most recent years prior to the implementation of the project activity |

5.7.2. Determination of $Q_{RD, y}$

$$Q_{RD,y} = Q_{VO,y} \times R_{RD} \times d_{RD}$$

Where:

| Q _{RD,y} | Amount of renewable diesel (tonnes) |
|------------------------|--|
| $Q_{VO,y}$ | = Amount of vegetable oil fed to HDS unit in year y (m ³) |
| R _{RD} | Ratio on volume basis of renewable diesel produced to vegetable oil fed to in the HDS unit (determined by carrying out a mass balance around the HDS unit or a laboratory test using relevant national or international standards) |
| d _{RD} | Density of renewable diesel (tonne/m³) |

Equation (17)

5.8. Changes required for methodology implementation in 2nd and 3rd crediting periods

60. The required changes shall be assessed using the tool for "Assessment of the validity of the current/original baseline and update of the baseline at the renewal of the crediting period".

5.9. Data and parameters not monitored

61. In addition to the parameters listed in the tables below, the provisions on data and parameters not monitored in the tools referred to in this methodology apply.

| Data / Parameter: | R _{RD} |
|-------------------------------------|---|
| Data unit: | m ³ renewable diesel / m ³ vegetable oil |
| Description: | Ratio between the amount of renewable diesel produced per vegetable oil fed into the HDS unit |
| Source of data: | Onsite measurements and calculations by the project participants |
| Measurement procedures (if any): | This parameter is to be determined by carrying out a mass balance around the HDS unit or a laboratory test using relevant national or international standards |
| Monitoring frequency: | This parameter is determined once and fixed throughout the crediting period |
| QA/QC procedures: | |
| Any comment: | |

Data / Parameter table 1.

Data / Parameter table 2.

| Data / Parameter: | d _{RD} |
|-------------------------------------|---|
| Data unit: | tonne/m ³ |
| Description: | Density of renewable diesel |
| Source of data: | Onsite measurements and calculations by the project participants |
| Measurement procedures (if any): | This parameter is to be estimated from (i) the density of the petrodiesel, (ii) the density of the petro/renewable diesel, and (iii) the volume fraction of renewable diesel (obtained by multiplying $Q_{VO,y}$ and R_{RD}) against petrodiesel (obtained by running the HDS unit only with gasoil) |
| Any comment: | This parameter is determined once and fixed throughout the crediting period |

Data / Parameter table 3.

| Data / Parameter: | EF _{CO2,PD} |
|-------------------------------------|--|
| Data unit: | tCO ₂ /TJ |
| Description: | CO ₂ emission factor of petrodiesel |
| Source of data: | IPCC default value at the lower limit of the confidence interval with 95% confidence level, as provided in Table 1.2 of Chapter 1 of Vol. 2 (Energy) of the 2006 IPCC Guidelines on National GHG Inventories |
| Measurement procedures (if any): | DDAET |
| Any comment: | |

Data / Parameter table 4.

| Data / Parameter: | EF co2,i |
|-------------------|--|
| Data unit: | tCO ₂ /TJ |
| Description: | CO ₂ emissions factor for fossil fuel type <i>i</i> |

| Source of data: | The following data sources may be used if the relevant conditions apply: | |
|-------------------------------------|--|---|
| | Data source | Conditions for using the data source |
| | (a) Values provided by the fuel supplier in invoices | This is the preferred source |
| | (b) Measurements by the project participants | If a) is not available |
| | (c) Regional or national default values | If a) is not available. |
| | default values | These sources can only be used for liquid fuels and should be based on well-documented, reliable sources (such as national energy balances) |
| | (d) IPCC default values at the upper limit of the uncertainty at a 95% confidence interval as provided in Table 1.2 of Chapter 1 of Vol. 2 (Energy) of the 2006 IPCC Guidelines on National GHG Inventories | If a) is not available |
| Measurement procedures (if any): | For (a) and (b): Measurements sh national or international fuel stand | |
| Any comment: | | |

Data / Parameter table 5.

| Data / Parameter: | VC _{H2,x} |
|-------------------------------------|---|
| Data unit: | Nm ³ |
| Description: | Volume of H ₂ consumed in the HDS unit in year x |
| Source of data: | Plant historical data |
| Measurement procedures (if any): | Flow meter at the inlet of the unit |
| Any comment: | - |

Data / Parameter table 6.

| Data / Parameter: | Q _{PD,x} |
|----------------------------------|--|
| Data unit: | m ³ |
| Description: | Amount of petrodiesel produced in year x |
| Source of data: | Plant historical data |
| Measurement procedures (if any): | Flow meter at the outlet of the unit |
| Any comment: | - |

Data / Parameter table 7.

| Data / Parameter: | FC _{NG,H2,x} |
|-------------------------------------|---|
| Data unit: | Nm ³ |
| Description: | Amount of natural gas consumed as fuel for H_2 production in year x |
| Source of data: | Plant historical data |
| Measurement procedures (if any): | - |
| Any comment: | - |

Data / Parameter table 8.

| Data / Parameter: | NCV _{NG,x} | | |
|----------------------------------|---|--|--|
| Data unit: | MJ/Nm ³ | | |
| Description: | Net calorific value of natural gas | combusted in year <i>x</i> | |
| Source of data: | The following data sources may b apply: | The following data sources may be used if the relevant conditions | |
| | Data source | Conditions for using the data source | |
| | (a) Values provided by the fuel supplier in invoices | This is the preferred source | |
| | (b) Measurements by the project participants | If a) is not available | |
| | (c) Regional or national default values | If a) is not available. These sources can only be used for liquid fuels and should be based on well-documented, reliable sources (such as national energy balances) | |
| | (d) IPCC default values at the upper limit of the confidence interval with 95% confidence level, as provided in Table 1.2 of Chapter 1 of Vol. 2 (Energy) of the 2006 IPCC Guidelines on National GHG Inventories | If a) is not available | |
| Measurement procedures (if any): | For (a) and (b): Measurements sh national or international fuel stand | | |
| Any comment: | - | | |

Data / Parameter table 9.

| Data / Parameter: | VP _{H2,x} |
|-------------------|---|
| Data unit: | Nm ³ |
| Description: | Volume of H ₂ produced in the H ₂ production facility in year x |
| Source of data: | Plant historical data |

| Measurement procedures (if any): | Flow meter at the outlet of the facility |
|-------------------------------------|--|
| Any comment: | - |

Data / Parameter table 10.

| Data / Parameter: | <mark>₿</mark> ₀ |
|-------------------------------------|--|
| <mark>Data unit:</mark> | <mark>tCH₄/tCOD</mark> |
| Description: | Maximum methane producing capacity |
| Source of data: | 2006 IPCC Guidelines for National GHG Inventories |
| Measurement procedures (if any): | The default IPCC value for B ₀ is 0.25 kgCH ₄ /kgCOD. Taking into account the uncertainty of this estimate, project participants should use a value of 0.265 kgCH ₄ /kgCOD as a conservative assumption for B ₀ |
| Any comment: | - |

Data / Parameter table 11.

| Data / Parameter: | MCF _P |
|--|---|
| <mark>Đata unit:</mark> | f raction |
| Description: | Methane conversion factor |
| Source of data: | The source of data should be the following, in order of preference: project specific data, country specific data or IPCC default values. As per guidance from the Board, IPCC default values should be used only when country or project specific data are not available or are difficult to obtain |
| <mark>Measurement</mark> procedures (if any): | - |
| A ny comment: | Preferably local specific value should be used. In absence of local values, MCFp default values can be obtained from table 6.3, chapter 6, volume 4 from 2006 IPCC Guidelines for National GHG Inventories |

Data / Parameter table 12.

| Data / Parameter: | GWP _{CH4} |
|-------------------------------------|---|
| Data unit: | tCO ₂ /tCH ₄ |
| Description: | Global warming potential of methane |
| Source of data: | IPCC |
| Measurement procedures (if any): | Default to be applied: 21 for the first commitment period. |
| Any comment: | This parameter shall be updated according to any future COP/MOP decisions |

Data / Parameter table 13.

| Data / Parameter: | EF co2,NG |
|-------------------|----------------------|
| Data unit: | tCO ₂ /TJ |

| Description: | CO ₂ emission factor of natural ga | s consumed |
|-------------------------------------|--|--------------------------------------|
| Source of data: | The following data sources may b apply: | be used if the relevant conditions |
| | Data source | Conditions for using the data source |
| | (a) Values provided by the fuel supplier in invoices | This is the preferred source |
| | (b) Measurements by the project participants | If (a) is not available |
| | (c) IPCC default values at the upper limit of the uncertainty at a 95% confidence interval as provided in Table 1.2 of Chapter 1 of Vol. 2 (Energy) of the 2006 IPCC Guidelines on National GHG Inventories | If (a) is not available |
| Measurement procedures (if any): | For (a) and (b): Measurements sh national or international fuel stand | |
| Any comment: | - | |

Data / Parameter table 14.

| BBAET | |
|----------------------------------|--|
| Data / Parameter: | |
| Data unit: | Nm ³ |
| Description: | Amount of natural gas used as feedstock for H_2 production in year x |
| Source of data: | Plant historical data |
| Measurement procedures (if any): | Flow meter at the inlet of the facility for feedstock |
| Any comment: | - |

6. Monitoring methodology

- 62. Describe and specify in the CDM-PDD all monitoring procedures, including the type of measurement instrumentation used and the responsibilities for monitoring and QA/QC procedures that will be applied. Where the methodology provides different options (e.g. use of default values or on-site measurements), specify which option will be used. Meters should be installed, maintained and calibrated according to equipment manufacturer instructions and be in line with relevant standards. If such standards are not available, use national standards. If a national standard is not available, then use international standards.
- 63. All monitoring should be attended to by appropriate and adequate personnel, as assessed by the project developer. All data collected as part of monitoring should be archived electronically and be kept at least for 2 years after the end of the last crediting period. 100% of the data should be monitored if not indicated otherwise in the tables below. All measurements should be conducted with calibrated measurement equipment according

to relevant industry standards. In addition, the monitoring provisions in the tools referred to in this methodology apply.

6.1. Data and parameters monitored

Data / Parameter table 15.

| Data / Parameter: | Exp _{PRD,An-I} |
|-------------------------------------|---|
| Data unit: | - |
| Description: | Export of the petro/renewable diesel to Annex I country |
| Source of data: | Sales records from the project participants |
| Measurement procedures (if any): | The DOE should verify that the petro/renewable diesel produced under the project activity are not exported to the Annex I country throughout the crediting period |
| Monitoring frequency: | - |
| QA/QC procedures: | - |
| Any comment: | The source of verification can be based on mass balance or sales records |

Data / Parameter table 16.

| Data / Parameter: | NCV _{PD,y} | |
|-------------------------------------|---|--|
| Data unit: | MJ/tonne | |
| Description: | Average net calorific value of petrodiesel in year y | |
| Source of data: | The following data sources may be used if the relevant conditions apply: | |
| | Data source Conditions for using the data source | |
| | (a) Measurements by the project participants This is the preferred source | |
| | (b) Regional or national default values If (a) is not available. These sources can only be used for liquid fuels and should be based on well-documented, reliable sources (such as national energy balances) | |
| | (c) IPCC default values at the upper limit of the confidence interval with 95% confidence level, as provided in Table 1.2 of Chapter 1 of Vol. 2 (Energy) of the 2006 IPCC Guidelines on National GHG Inventories | |
| Measurement procedures (if any): | For (a): Measurements should be undertaken in line with national or international fuel standards | |

| Monitoring frequency: | For (a): Monthly, averaged for the year For (b) and (c): Annually |
|-----------------------|--|
| QA/QC procedures: | Verify that the values under (a) and (b) are within the uncertainty range of the IPCC default values as provided in Table 1.2, Vol. 2 of the 2006 IPCC Guidelines. If the values out of this range, collect additional information from the testing laboratory to justify the outcome or conduct additional measurements. The laboratories in (a) or (b) should have ISO17025 accreditation or justify that they can comply with similar quality standards |
| Any comment: | - |

Data / Parameter table 17.

| Data / Parameter: | Qvo,y |
|-------------------------------------|--|
| Data unit: | m ³ |
| Description: | Amount of vegetable oil fed to HDS unit in year y (m ³ VO) |
| Source of data: | Onsite measurements by the project participants |
| Measurement procedures (if any): | The volume of vegetable oil fed into HDS unit shall be monitored by the flow meter at the inlet of the unit |
| Monitoring frequency: | Continuously, data is presented as hourly average |
| QA/QC procedures: | The flow meter will be calibrated according to the suppliers' specifications and following the refinery QA/QC procedures. |
| Any comment: | In case the production of renewable/petrodiesel is seasonal, such parameter will be monitored continuously only when vegetable oil is introduced in the HDS unit |

Data / Parameter table 18.

| Data / Parameter: | NCV _{NG,y} | |
|-------------------|--|---|
| Data unit: | MJ/Nm ³ | |
| Description: | Average net calorific value of the | natural gas combusted in year y |
| Source of data: | The following data sources may be used if the relevant conditions apply: | |
| | Data source | Conditions for using the data source |
| | (a) Values provided by the fuel supplier in invoices | This is the preferred source |
| | (b) Measurements by the project participants | If (a) is not available |
| | (c) Regional or national default values | lf (a) is not available. |
| | | These sources can only be used for liquid fuels and should be based on well-documented, reliable sources (such as national energy balances) |
| | (d) IPCC default values at the upper limit of the | If (a) is not available |
| | confidence interval with | |

| | 95% confidence level, as provided in Table 1.2 of Chapter 1 of Vol. 2 (Energy) of the 2006 IPCC Guidelines on National GHG Inventories |
|----------------------------------|--|
| Measurement procedures (if any): | For (a) and (b): Measurements should be undertaken in line with national or international fuel standards |
| Monitoring frequency: | For (a): Each batch of fuel supplied, averaged for the year For (b): Monthly, averaged for the year For (c) and (d): Annually |
| QA/QC procedures: | Verify that the values under (a), (b) and (c) are within the uncertainty range of the IPCC default values as provided in Table 1.2, Vol. 2 of the 2006 IPCC Guidelines. If the values out of this range, collect additional information from the testing laboratory to justify the outcome or conduct additional measurements. The laboratories in (a), (b) or (c) should have ISO17025 accreditation or justify that they can comply with similar quality standards |
| Any comment: | - |

Data / Parameter table 19.

| Data / Parameter: | VC _{H2,y} |
|-------------------------------------|---|
| Data unit: | Nm ³ |
| Description: | Volume of H_2 consumed in the HDS unit in the year y |
| Source of data: | Onsite measurements by the project participants |
| Measurement procedures (if any): | The volume of H_2 consumed in the HDS unit shall be monitored by the flow meter at the inlet of the unit |
| Monitoring frequency: | Continuously, data is presented as hourly average |
| QA/QC procedures: | The flow meter will be calibrated according to the suppliers' specifications and following the refinery QA/QC procedures |
| Any comment: | In case the production of petro/renewable diesel is seasonal, such parameter will be monitored continuously only when vegetable oil is introduced in the HDS unit |

Data / Parameter table 20.

| Data / Parameter: | Q _{PRD,y} |
|----------------------------------|--|
| Data unit: | m ³ |
| Description: | Total amount of petro/renewable diesel produced by the project activity in year y (m ³) |
| Source of data: | Onsite measurements by the project participants |
| Measurement procedures (if any): | Total amount of petro/renewable diesel produced shall be monitored by the flow meter at the outlet of the HDS unit |
| Monitoring frequency: | Continuously, data is presented as hourly average |
| QA/QC procedures: | The flow meter will be calibrated according to the suppliers' specifications and following the refinery QA/QC procedures |

Data / Parameter table 21.

| Data / Parameter: | ηH2,react,y |
|-------------------------------------|--|
| Data unit: | Fraction |
| Description: | Reaction efficiency of H_2 formation in year y |
| Source of data: | Default factor or onsite measurements by the project participants |
| Measurement procedures (if any): | The project participants can use a conservative default value of 1 or can calculate it considering the stoichiometry of the reaction to produce H_2 and the actual amount of end products obtained and document transparently in the CDM-PDD. Measurements should be undertaken in line with national or international standards |
| Monitoring frequency: | Monthly |
| QA/QC procedures: | - |
| Any comment: | - |

Data / Parameter table 22.

| Data / Parameter: | NCV _{i,y} | | |
|-------------------|--|--|--|
| Data unit: | MJ/tonne | | |
| Description: | Net calorific value of fossil fuel type <i>i</i> in year <i>y</i> | | |
| Source of data: | The following data sources may be used if the relevant conditions apply: | | |
| | Data source Conditions for using the data source | | |
| | (a) Values provided by the fuel supplier in invoices | | |
| | (b) Measurements by the If (a) is not available project participants | | |
| | (c) Regional or national default valuesIf (a) is not available.These sources can only be used for liquid fuels and should be based on well-documented, reliable sources (such as national energy balances) | | |
| | (d) IPCC default values at the upper limit of the confidence interval with 95% confidence level, as provided in Table 1.2 of Chapter 1 of Vol. 2 (Energy) of the 2006 IPCC Guidelines on National GHG InventoriesIf (a) is not available | | |

| Measurement procedures (if any): | For (a) and (b): Measurements should be undertaken in line with national or international fuel standards |
|-------------------------------------|--|
| Monitoring frequency: | For (a): Each batch of fuel supplied, averaged for the year For (b): Monthly, averaged for the year For (c) and (d): Annually |
| QA/QC procedures: | Verify that the values under (a), (b) and (c) are within the uncertainty range of the IPCC default values as provided in Table 1.2, Vol. 2 of the 2006 IPCC Guidelines. If the values out of this range, collect additional information from the testing laboratory to justify the outcome or conduct additional measurements. The laboratories in (a), (b) or (c) should have ISO17025 accreditation or justify that they can comply with similar quality standards |
| Any comment: | - |

Data / Parameter table 23.

| Data / Parameter: | Q _{WW,d,y} |
|--|--|
| <mark>Data unit:</mark> | <mark>∰</mark> ³ |
| Description: | Amount of wastewater treated anaerobically or released untreated from the vegetable oil production plant on day <i>d</i> in year y |
| Source of data: | Onsite measurements by the project participants |
| <mark>Measurement</mark> p rocedures (if any): | Amount of wastewater treated anaerobically or released untreated from the vegetable oil production plant shall be monitored by the flow meter at the outlet of vegetable oil production facility wastewater stream |
| Monitoring frequency: | Continuously, data is presented as daily average |
| QA/QC procedures: | The flow meter will be calibrated according to the suppliers' specifications and following the refinery QA/QC procedures |
| A ny comment: | If the wastewater is treated aerobically, emissions are assumed to be zero, and hence this parameter does not need to be monitored. For the days when the vegetable oil production plant is not operational, the value is zero for this parameter for that particular day |

Data / Parameter table 24.

| Data / Parameter: | СОР _{WW,d,y} |
|---|--|
| <mark>Data unit:</mark> | t <mark>COD/m³</mark> |
| Description: | Chemical Oxygen Demand (COD) of wastewater on day <i>d</i> in year y |
| Source of data: | Onsite measurements by the project participants |
| <mark>Measurement</mark> procedures (if any): | COD of wastewater shall be monitored at the outlet of vegetable oil production plant wastewater stream following national or international standards |
| Monitoring frequency: | <mark>Daily</mark> |
| QA/QC procedures: | |

| Any comment: | If the wastewater is treated aerobically, emissions are assumed to be zero, and hence this parameter does not need to be monitored. |
|--------------|--|
| | For the days when the vegetable oil production plant is not operational, the value is zero for this parameter for that particular day |

Data / Parameter table 25.

| Data / Parameter: | A _{s,y} |
|-------------------------------------|--|
| Data unit: | ha |
| Description: | Area in which oil seed type s is cultivated for use in the project plant in year y |
| Source of data: | Onsite measurements by the project participants |
| Measurement procedures (if any): | Measure the area in which oil seed type s is cultivated for each plantations and use the largest area among all the plantations in year y for this parameter |
| Monitoring frequency: | Each plantation |
| QA/QC procedures: | - |
| Any comment: | - |

Data / Parameter table 26.

| Data / Parameter: | AF _y | |
|----------------------------------|--|--|
| Data unit: | Fraction D C | |
| Description: | Allocation factor for the oil seeds cultivation in year y | |
| Source of data: | - | |
| Measurement procedures (if any): | Estimated as per the TOOL25 "Guidance on apportioning of emissions to co-products and by-products" | |
| Monitoring frequency: | Annually | |
| QA/QC procedures: | - | |
| Any comment: | | |

Appendix 1. Determination of factor F in the production of Hydrogen

- 1. Fuel is combusted to supply energy to the reactor where H_2 is generated by reforming natural gas with steam. The other emission source related to H_2 production is represented by the chemical reaction that occurs when H_2 is generated.
- 2. The reforming of natural gas with steam is the process used to generate H₂. The chemical reactions are:

$$CH_4 + H_2O \rightarrow CO + 3H_2$$
 Equation (1)

Equation (2)

 $CO + H_2O \rightarrow CO_2 + H_2$

- 3. The *F* factor used in Equation (9) is obtained as follows:
 - (a) As the volume of H₂ required by the HDS unit to process a certain amount of vegetable oil is known in the refinery activity, the proposed methodology uses this value to obtain the mass of CO₂ produced in the chemical reaction that forms H₂.
 - (b) To obtain the mass of CO₂ generated in the chemical reaction using the volume of H₂ required by the hydrogenation process, the *"ideal gas equation"* is applied as follows:

$$n_{H_2} = \frac{P_{H_2} \times V_{H_2}}{R \times T_{H_2}}$$
 Equation (3)

Where:

| п _{Н2} | = Number of moles of H ₂ produced in the reaction (mol) |
|------------------------|--|
| R | = 8.314 (m³ Pa/K mol) |
| V _{H2} | = Volume of H ₂ produced in the reaction (Nm ³) |
| Т | = 273 (K), temperature of gases in normal conditions |
| P _{H2} | = 101,325 (Pa), pressure of gases in normal conditions |

4. Naming "a" the constant that multiplies the volume of H₂, the abovementioned "*ideal gas equation*" yields:

$$n_{H_2} = a \times V_{H_2}$$
 Equation (4)

Where:

$$a = 44.6 \text{ (mol/Nm}^3)$$

5. Based on the stoichiometry of the reaction of H₂

$$CH_4 + 2H_2O \rightarrow CO_2 + 4H_2$$
 Equation (5)

The number of moles of CO_2 emitted per mole of H_2 produced is:

$$n_{CO_2} = \frac{1}{4} \times n_{H_2}$$
 Equation (6)

6. Substituting Equation (4) in Equation (6):

$$n_{CO_2} = \frac{a}{4} \times V_{H_2}$$
 Equation (7)

7. To obtain the mass of CO_2 produced in the reaction, it is necessary to multiply Equation (7) by the molar mass of carbon dioxide, as follows:

$$n_{CO_2} = M_{CO_2} \times \frac{a}{4} \times n_{H_2}$$
 Equation (8)

Where:

 M_{CO2} = Molar mass of CO₂, equal to 44 g/mol

8. Thus, the *F* factor becomes:

$$F = \frac{44.6 \times 44}{4} = 490.6$$
 Equation (9)

- 9. As the H₂ chemical formation reaction is not 100 per cent efficient the factor *F* must be multiplied by $\eta_{reaction}$, which is the efficiency of the H₂ formation reaction.
- 10. Thus, the *F* factor used in Equation (9) is:

$$F = 490.6 \times \eta_{reaction}$$
 Equation (10)

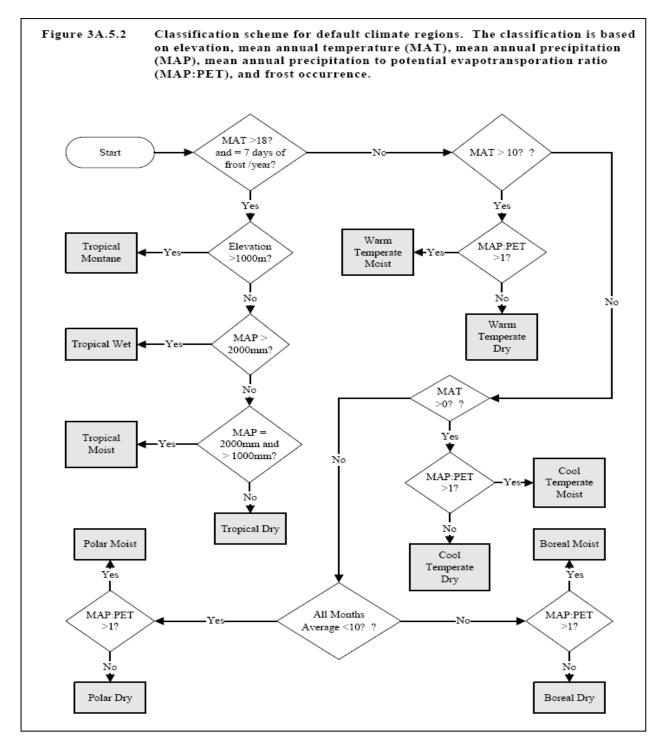
11. And, the mass of CO_2 produced in the chemical formation reaction of H_2 is:

$$m_{CO_2} = 490.6 \times \eta_{reaction} \times V_{H_2}$$
 Equation (11)

Where:

| <i>m</i> _{CO2} | = | Mass of CO ₂ (g) |
|-------------------------|---|---|
| V _{H2} | = | Volume of H_2 produced in the reaction (Nm^3) |

Appendix 2. Climate Zone



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Document information

| Version | Date | Description |
|---------|-------------------|--|
| 03.0 | 21 February 2022 | MP 87, Annex 7 |
| | | To be considered by the Board at EB 113. |
| | | A call for public input will be issued for this draft document. Any input will be discussed with the MP and forwarded to the Board for its consideration together with this document. |
| | | Revision to indicate the emission sources that are relevant in the calculation of project emissions associated with biomass and biomass residues, in line with the draft revision of the "TOOL16: Project and leakage emissions from biomass". |
| 02.0 | 24 July 2015 | EB 85, Annex 7 |
| | | Revision to: |
| 01.1 | 26 November 2010 | Add a reference to the following methodological tools: (a) "Upstream leakage emissions associated with fossil fue use"; (b) "Assessment of the validity of the original/currer baseline and update of the baseline at the renewal of the crediting period"; (c) Project and leakage emissions from transportation of freight; (d) Project emissions from cultivation of biomass. Clarify that net leakage should always be considered as zero when net leakage effects are negative; Change the sectoral scope of the methodology from 01 and 05 to 05, 13 and 15; Editorial improvement. |
| 01.1 | 26 November 2010 | EB 58, Annex 6 Revision to exclude the consumers from the project boundary. |
| 01.0 | 17 September 2010 | EB 56, Annex 3 |
| | | Initial adoption. |

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