



**CLEAN DEVELOPMENT MECHANISM
PROJECT DESIGN DOCUMENT FORM (CDM-PDD)
Version 03 - in effect as of: 28 July 2006**

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**SECTION A. General description of project activity****A.1 Title of the project activity:**

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Jiratpattana Biogas Energy Project

14/07/08

Version 03.1

A.2. Description of the project activity:

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The Jiratpattana Biogas Energy Project (hereafter, the Project) developed by Thai Biogas Energy Company Ltd (hereafter referred to as “TBEC, ”or the Project Developer) is an anaerobic digestion project, which treats wastewater from the cassava processing factory owned by Jiratpattana Agriculture Limiteds (hereafter referred to as the Facility) in Kalasin, Thailand. In the baseline scenario, the wastewater flows from the factory through a series of 9 low-maintenance anaerobic and aerobic lagoons. As the wastewater flows through the lagoons, organic material is broken down and resulting methane is released to the atmosphere.

In the Project Activity, a Covered In-Ground Anaerobic Reactor (CIGAR) will be installed before the lagoon series; the CIGAR remove the organic material in the wastewater, thus reducing the Chemical Oxygen Demand (COD) and subsequent fugitive CH₄ emissions. Biogas produced in the CIGAR will be used in the Jiratpattana Agriculture Limited factory to dry the wet starch cake to the final dry starch product, thereby displacing the over 6 million litres of fuel oil currently employed to dry the starch product. Excess biogas will be utilised in generators to produce electricity and will displace electricity from the Thai National Grid. Two gensets of 1.05 MW capacity will be installed. Further generation capacity may be added, with excess generation to be exported to the grid when Power Purchase Agreements (PPAs) can be negotiated with the local utility. Surplus biogas, where produced, will be flared rather than released to the atmosphere.

	Baseline Scenario	Project activity
Wastewater Treatment	Wastewater, high in COD, is treated via a lagoon system, producing methane-rich biogas	A Covered In-Ground Anaerobic Reactor-CIGAR- will be used to treat this wastewater, reducing the water's COD prior to release to the current pond system
Industrial Activities	Use of fuel oil to dry wet tapioca starch cake	Use of renewable, sustainably produced biogas in dual fuel burner system to ensure heating energy self-sufficiency
	Use of grid electricity	Generation of electricity from surplus biogas

The project is helping the Host Country fulfil its goals of promoting sustainable development. Specifically:



- The project will act as a clean technology demonstration project, which could be replicated across Thailand and the region;
- It will act as an important capacity building project, nationally and locally, especially demonstrating the use of a new financial mechanism for funding of the renewable energy and waste management sector via the CDM;
- It increases diversity and security of energy supplied through energy self-sufficiency, reducing the import of energy from overseas - with a positive effect on Thailand's balance of payment;
- The project creates temporary employment opportunities during construction and permanent employment opportunities during operation;
- It provides additional value for cassava production through energy production;
- The project will make use of material currently considered a waste material that gives rise to a considerable hazard i.e. the flammable methane rich biogas emitted;
- Technology will be sourced locally where possible, or transferred from overseas where required.

A.3. Project participants:

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Project participants

Name of party involved (*) ((host) indicates a host party)	Private and/or public entity(ies) Project participants (*) (as applicable)	Kindly indicate if the party involved wishes to be considered as project participant (Yes/No)
Kingdom of Thailand	Thai Biogas Energy Company	No
United Kingdom of Great Britain and Northern Ireland	EcoSecurities Group plc	No

A.4. Technical description of the project activity:**A.4.1. Location of the project activity:**

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A.4.1.1. Host Party(ies):

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Thailand (the "Host Country")

A.4.1.2. Region/State/Province etc.:

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Kalasin Province

A.4.1.3. City/Town/Community etc:

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Phudin, Muang

A.4.1.4. Detail of physical location, including information allowing the unique identification of this project activity (maximum one page):



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Jiratpattana Agriculture Limited Project, 208 39 Moo 4 Kalasin-Sahasakhan Road, Phudin, Muang, Kalasin, 46000, Thailand. The GPS coordinates: 16°37'01.02"N 103°30'45.86"E

A.4.2. Category(ies) of project activity:

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The project sectoral scope, as defined by the UNFCCC, is: 13 - Waste handling and disposal.

A.4.3. Technology to be employed by the project activity:

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The project will involve three important components, each requiring the transfer of technology, each at different stages of characterisation in the region and worldwide.

- 1. Fugitive Methane Mitigation:** The primary emissions reduction component stems from capturing fugitive methane emissions through a Covered In-Ground Anaerobic Reactor, a type of anaerobic digester, which consists of a series of baffled reactors connected only by overflow weirs. The CIGAR may include a final settling unit. The CIGAR was first developed by Waste Solutions Ltd. in New Zealand. In addition to the anaerobic digester itself, the CIGAR consists of a piping system that moves the biogas from the digester to the flare, gen sets and dual fuel burner, as well as a state-of-the-art monitoring system.
- 2. Fuel Switching to use Biogas:** In the project activity, heat will be generated in two boilers – a Wiesloch and Bertrams Konus. Each of the boilers have a capacity of 3,663 kW thermal. The burners are RGMS50/2-A Weishaupt burner.
- 3. Electricity Generation to use Biogas:** Two 1046kW JGC 320 GS B.L GE Jenbacher gensets will generate electricity onsite. The GE Jenbacher is specifically designed to run on methane-rich biogas.

Any excess biogas will be sent to a flare. The flare is an Organics Ltd. Flare with a capacity of 2000 Nm³ per hour. The flame is detected by a UV sensor.

A.4.4. Estimated amount of emission reductions over the chosen crediting period:

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The table below sets out the emissions profile of the project over the ten-year crediting period.

Total Emissions Reductions throughout the Crediting Period (tCO₂e)



Years	Annual estimation of emissions reductions (tonnes of CO ₂ e)
2009	24,726
2010	24,726
2011	24,726
2012	24,726
2013	24,726
2014	24,726
2015	24,726
2016	24,726
2017	24,726
2018	24,726
Total Estimated Reductions (tonnes of CO ₂ e)	247,264
Total Number of Crediting Years	10
Annual average of the crediting period of emissions reductions (tonnes of CO ₂ e)	24,726

A.4.5. Public funding of the project activity:

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The project will not receive any public funding from Parties included in Annex I of the UNFCCC.

SECTION B. Application of a baseline and monitoring methodology**B.1. Title and reference of the approved baseline and monitoring methodology applied to the project activity:**

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AM0022 Avoided Wastewater and On-site Energy Use Emissions in the Industrial Sector, Version 04 (EB 28). AMS I.D. version 12 (EB 33) was used to calculate the grid emission factor. The “Tool to determine project emissions from flaring gases containing methane” (EB 28) will be used to calculate project emission from flaring.

B.2 Justification of the choice of the methodology and why it is applicable to the project activity:



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AM0022 specifically focuses on wastewater fugitive methane abatement through anaerobic digestion in an industrial context. AM0022 sets out the following applicability criteria, and evidence for the Project meeting those criteria is listed below:

Methodology Conditionality

Condition	Applicable?	Justification / Project Condition
Project is implemented based upon a baseline of existing lagoon-based industrial wastewater treatment facilities for wastewater with high organic loading;	Yes	Jiratpattana Biogas Energy Project currently uses an anaerobic lagoon system to manage the high organic load of the wastewater.
The methodology is applicable only to the improvement of existing wastewater treatment facilities. It is not applicable for new facilities to be built, or new build to extend current site capacity;	Yes	The lagoon system at Jiratpattana Biogas Energy Project has been in operation for several years, since the factory began operation. The project activity will not lead to an increase in production capacity.
The organic wastewater contains simple organic compounds (monosaccharides);	Yes	The facility processes cassava which by nature contains simple organic compounds ¹ .
It can be shown that the baseline is the continuation of a current lagoon system for managing wastewater. In particular, the current lagoon-based system is in full compliance with existing rules and regulations	Yes	The existing lagoon system is in full compliance with all current regulations in Thailand ² .
The depth of the anaerobic lagoon should be at least 1 m	Yes	The depth of the anaerobic lagoon is greater than 1 m (approximately 4-5m).
The temperature of the wastewater in the anaerobic lagoons is always at least 15 °C	Yes	The average ambient temperature in the region is 25 °C ³ ; the wastewater temperature is at least this as it is not cooled in any manner.
In the project, the biogas recovered from the anaerobic treatment system is flared and/or used onsite for heat and/or power generation, surplus biogas is flared	Yes	Biogas is used onsite in the facilities' heaters and for the purpose of electricity generation. Surplus biogas is flared.
Heat and electricity needs per unit input of the water treatment facility remain largely unchanged before and after the project;	Yes	The project will not require any significant increase in heat or electricity needs. The energy requirements for the project activity are minimal.

¹ Reducing sugar testing was completed to demonstrate that the wastewater contains simple organic compounds.

² A certificate from the Provincial Government certifying compliance with regulations and COD testing results were made available to the validator.

³ www.weather.co.uk



Data requirements as laid out in the related Monitoring Methodology are fulfilled. In particular, organic materials flow into and out of the considered lagoon based treatment system and the contribution of different removal processes can be quantified (measured or estimated).	Yes	The monitoring plan based on the Monitoring Methodology has been implemented onsite. All data - including the monitoring of wastewater volume, organic content at the inlet and outlet of the digester, and contribution of removal processes - required to be tested is accurately measured or estimated, in accordance with AM0022, version 04. For further details, refer to section B.7.
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B.3. Description of the sources and gases included in the project boundary

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According to AM0022, project boundaries should be drawn encompassing:

- Methane emissions from the existing lagoon-based waste water treatment system up to, and including, the point at which organic material flows can be quantified or estimated into and out of the wastewater treatment facility;
- Potential methane emissions from the newly introduced anaerobic waste water treatment facility;
- CO₂ emissions from displaced fuel oil historically used for on site heat generation at the Jiratpattana Agriculture Limited Partnerships facility;
- CO₂ emissions from displaced fuel oil used for generation of grid electricity that would otherwise have been consumed from the Thai National grid;
- Methane emissions from incomplete combustion of biogas in heat and/or power generation or in flare systems, or from leakage in piping.

In accordance with AM0022, emissions that are not considered include: nitrous oxide from the waste treatment system, and nitrous oxide from biogas combustion and/or destruction.

The following project activities and emission sources are considered within the project boundaries:

Sources and gases included in the project boundary

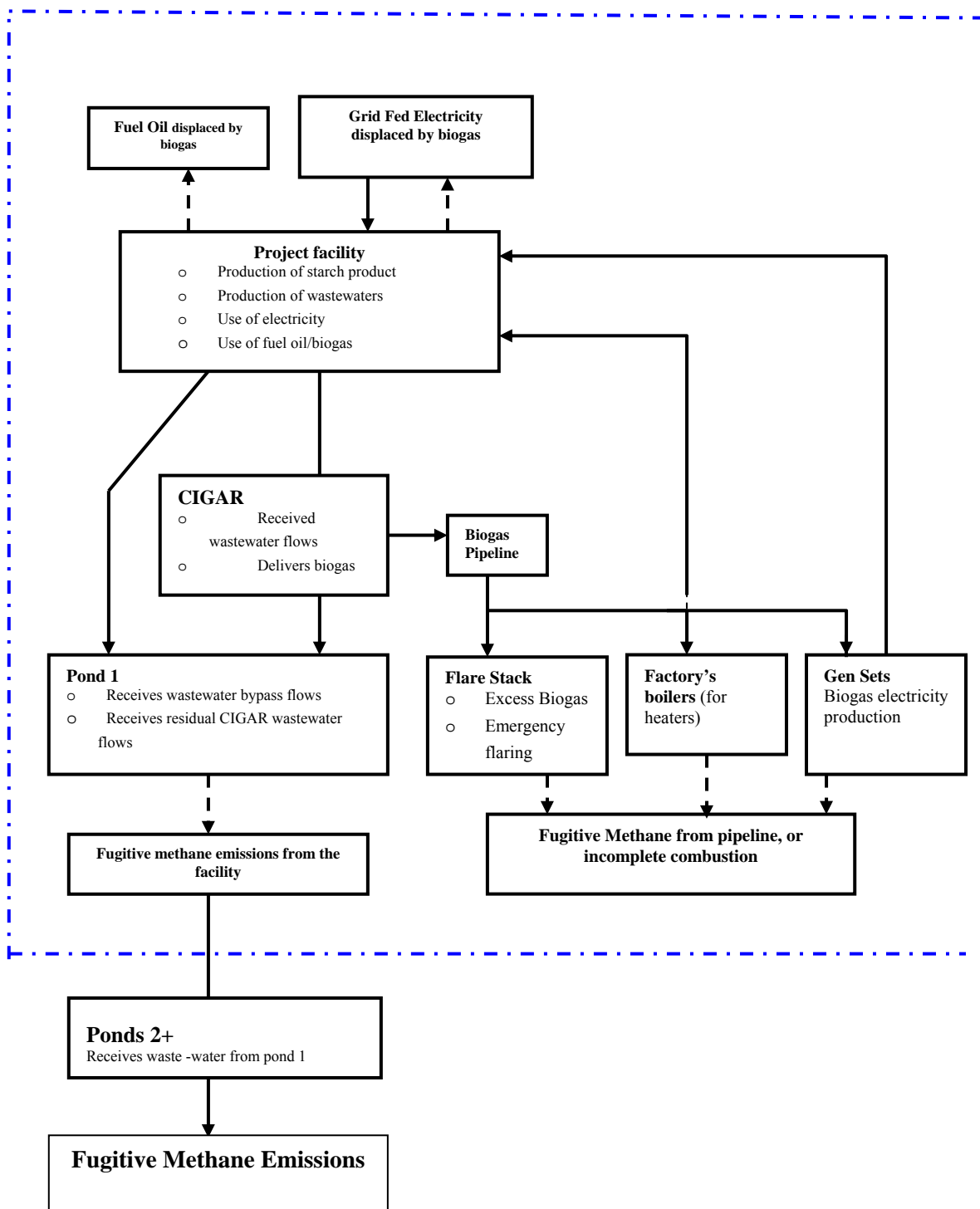
	Source	Gas	Included?	Justification/Explanation
Baseline	Existing lagoon-based waste water treatment system	CO ₂	No	CO ₂ is not considered in the lagoon-based wastewater treatment.
		CH ₄	Yes	In accordance with AM0022, CH ₄ is the only gas considered in the lagoon-based wastewater treatment.
		N ₂ O	No	Not applicable
	Emissions from displaced fossil fuel use for onsite heat generation	CO ₂	Yes	In accordance with AM0022, only CO ₂ is considered in the emissions from displaced fuel oil.
		CH ₄	No.	CH ₄ is not considered in the emissions from displaced fossil fuel.



		N ₂ O	No	Not applicable
	Emissions from displaced fossil fuel use for grid generation of electricity that would otherwise have been produced	CO ₂	Yes	In accordance with AM0022, CO ₂ is the only gas considered in the emissions from displaced fossil fuel used in the electricity grid.
		CH ₄	No	CH ₄ is not considered in the emissions from displaced fossil fuel used in the electricity grid.
Project Activity	Existing lagoon-based waste water treatment system	N ₂ O	No	Not applicable
		CO ₂	No	CO ₂ from the lagoons is not a source of project emissions.
		CH ₄	Yes	In accordance with AM0022, CH ₄ from the lagoons is the only gas considered as a source of project emissions.
	Emissions from leakage in piping	N ₂ O	No	Not applicable
		CO ₂	No	Not applicable
		CH ₄	Yes	CH ₄ emissions from leakage in piping will be considered as according to AM0022.
	Fugitive Emissions from the Flare	N ₂ O	No	Not applicable
		CO ₂	No	CO ₂ from combustion is not accounted for in Project Emissions.
		CH ₄	Yes	In accordance with AM0022, methane emissions due to incomplete combustion are accounted for in Project Emissions.
	Fugitive Emissions from the Gen Set	N ₂ O	No	Not Applicable
		CO ₂	No	CO ₂ from combustion is not accounted for in Project Emissions.
		CH ₄	Yes	Methane emissions due to incomplete combustion are accounted for in Project Emissions.
	Fugitive Emissions from the Dual Fuel Burner	N ₂ O	No	Not Applicable
		CO ₂	No	CO ₂ from combustion is not accounted for in Project Emissions.
		CH ₄	Yes	Methane emissions due to incomplete combustion are accounted for in Project Emissions, as according to AM0022.
		N ₂ O	No	Not Applicable



Jiratpattana Biogas Energy Project



**B.4. Description of how the baseline scenario is identified and description of the identified baseline scenario:**

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As according to AM0022, a six step process was used in order to define the baseline and to demonstrate the continuation of current practices (existing lagoon based waste water treatment system without biogas use or flaring of the biogas).

Step 1: List a range of potential baseline option:

1. Continuation of current practices (BAU);
2. Direct release of wastewaters to an offsite water way;
3. Anaerobic digestion of wastewater streams;
4. Aerobic treatment of wastewaters (activated sludge or filter bed type treatment).

Step 2: Identify significant potential barrier:

- Legal;
- Technical;
- Financial;
- Social;
- Business culture;

Step 3: Score the barrier:

Legal

- Is this practice regulated by Host Nation law or regulation and therefore legally allowed?

Are there legal barriers to alternative baseline practices?

- Current practice: **No.**
 - This activity is not regulated by national law, and is therefore legal.
- Direct Discharge to water bodies: **Yes.**
 - This option is not allowed under Thai law. There will be no further discussion of this option in the barriers analysis.
- Anaerobic digestion: **No.**
 - No law exists to drive an alternative waste management practice. This activity is not regulated by national law, and is therefore legal.
- Aerobic treatment: **No.**
 - No law exists to drive an alternative waste management practice. This activity is not regulated by national law, and is therefore legal.

There are no laws or regulations regulating the use of pond systems, the current practice (BAU), anaerobic digestion of wastewater streams or aerobic treatment of wastewaters in Thailand. However, the Enhancement and Conservation of National Environmental Quality Act of 1992 prohibits direct release into water bodies (rivers, lakes etc). As an option that contravenes the law cannot be considered realistic, the regulation for the purposes of this project can be considered an absolute barrier. Hence, the option of



directly releasing wastewaters to an offsite water way is not discussed further throughout the barriers analysis.

In the case of the Project, there is an extensive lagoon system that functions in COD removal and, ultimately, evaporation of the wastewater flow. Therefore, under the BAU scenario, there is no need for discharge to the environment. No permit is required for this system (as there is no discharge). Furthermore, Thailand does not require the monitoring of CO₂, CH₄, or any other GHG emissions and thus fugitive methane emissions from the lagoon system are not held to any standard of compliance.

Current practice, anaerobic and aerobic treatment of wastewaters would represent legal management options and would not be subject to additional regulation, apart from that they need to achieve the same effluent release standards as in the current pond systems.

Legal issues are therefore not considered a barrier to any of the scenarios, other than the direct discharge of water bodies.

Technical

- Is this technology option currently available through local equipment suppliers?
- Are there sufficient skills and labour to operate and maintain this technology in country?
- Is this technology a regional or global standard, or technology of choice?
- Can performance certainty be guaranteed within tolerance limits?
- Can real or perceived technology risk associated with this technology be discounted?

Are there technical barriers to alternative baseline practices?

- Current practice: **No.**
 - This technology is the technology of choice in Thailand and the region.
- Anaerobic digestion: **Yes.**
 - This is perceived as a risky, novel and locally unavailable technology. Few AD plants existed in Thailand prior to the implementation of the Project.
- Aerobic treatment: **Yes.**
 - In the industrial sector regionally, little aerobic treatment is employed on a commercial scale.

Pond based wastewater cleansing systems have low capital and O&M costs and are a low maintenance solution. These types of systems are used extensively both in Thailand and world wide (Parr, Smith and Shaw 2000). Ponds are the technology of choice in tropical situations and any other area where regulation does not require more engineered solutions. They are seen as very low risk, and utilise low-tech pond redundancy to ensure that final releases of wastewater effluents are within regulated tolerances.

Anaerobic systems are novel, not only in Thailand, but the wider region and globally. Neither the technology, nor the requisite skills to build and operate such systems are generally available locally. The majority of the equipment used in the Project activity had to be purchased from overseas as it was not available in Thailand. Additionally, due to the lack of utilization of anaerobic digestion technology in Thailand, there is a lack of skilled labourers to operate and maintain this technology. Furthermore, it is hard to attract interest to work in the field (Prasertsan, Sajjakulnukit 2005).



Skilled labourers must be trained on the O&M procedures of digesters, especially CIGARs. This training was conducted by Waste Solutions Limited, a New Zealand based company⁴.

Furthermore, at the time of writing, there are only 5MW of electricity being generated in Thailand from biogas and this is from a registered CDM project activity and two other proposed CDM activities (Biopact 2007).

AD systems are perceived as relatively high risk, being based upon the function of a biological system that is neither 100% characterised, nor performance guaranteed. The biological system is at constant risk of changes in the chemical composition that can harm the anaerobic bacteria and biological activity and subsequently the waste management and energy production regimes. These harmful changes can be caused by a host of problems such as mismanagement of the CIGAR or mixing pond, improper recycling of the wastewater or the introduction of chemical agents into the system. AD systems require constant and ongoing precise management of a variety of elements, water flows, pH etc. Overall they are perceived as a risky solution.

Aerobic management systems are similarly a novel choice in Thailand; the majority of wastewater treatment systems are anaerobic lagoons, as demonstrated above. Aerobic treatment systems are not very common. They are complicated to control and costly due to the high energy requirement (oxygen needs to be supplied) and a large volume of sludge is produced (Parr, Smith and Shaw 2000). Oxygen is supplied to the system through a mechanical process; the necessary operating and maintenance of this mechanical system is much greater than that of the use of anaerobic lagoons. Furthermore, the significant amount of sludge generated by aerobic systems must be disposed of.

Technology issues are therefore considered a major barrier to the anaerobic scenario and mid-range barrier to the aerobic alternative and no barrier to the current pond based management system.

Financial

- Is this technology intervention financially attractive in comparison to other technologies?
- Is this the most financially viable option?
- Is equity participation easy to find internationally?
- Is equity participation easy to find locally?
- Are site owners/ project beneficiaries carrying any risk?
- Is technology currency (country) denomination a risk?
- Is the proposed project subject to commercial risks?

Are there financial barriers to alternative baseline practices?

- Current practice: **No.**
 - This technology, where currently installed, requires no further financing.
- Anaerobic digestion: **Yes.**
 - This is perceived as a high risk, novel project. No successful commercial AD plants exist in Thailand at present that have not been developed outside the CDM. In this project, no risk is being taken by Thai nationals or the facility management, the risk being left to niche foreign investors.
- Aerobic treatment: **Yes.**

⁴ Please refer to Annex 6 for proof of training by Waste Solutions Ltd



- Similar risks (although perhaps lower) may be observed for aerobic treatment.

In discussing financial analysis of any project that involves – or could involve - multiple parties with distinct roles, a key variable to consider is the relative division of risk and reward between those parties.

For the facility, the current system is financially attractive, given that it complies with current regulation and requires virtually no management input to achieve the key parameter. For the facility, ponds represent the lowest cost of all three scenarios i.e. making it the most financially viable option since even the most productive land in developing countries is reasonably priced, which ensures the feasibility of waste stabilization ponds as a sustainable alternative for wastewater treatment (Peña Varón 2003). The current system requires no further costs while the implementation of the project activity incurs significant costs⁵. Under this scenario, the facility's unit energy costs would remain on par with the rest of the industry, leaving it at no relative competitive disadvantage.

Commercial risk is a very significant barrier to adopting waste to energy AD technology. The commercial risks include 1) complete non-performance or dissatisfactory biogas yield insufficient to offset the high Operation & Maintenance costs and depreciation⁶ 2) cost overruns to already high capex budgets 3) biological shocks that harm or kill the bacteria interrupting cash flows 3) business risk of host company that can't be controlled by project developer, directly affect the CIGAR 4) lack of control of the starch produced by Host Company as even small changes in the starch product may affect the biogas yield significantly. This is exemplified by the comparison of the overall risks associated with maintaining the business as usual scenario (no risk) against the risks associated with project implementation even if the risk, which is high, is borne by a number of different entities. There is further investment risk due to the risk associated with the vulnerability of the Thai baht. Sentiment towards the baht is undermined by domestic political instability and signs of slower economic growth (Economist Intelligence Unit 2006).

The project activity was not able to get funding from any Thai sources; it is only able to proceed due to being financed exclusively by equity from foreign investors specializing in high-risk projects. For example, Al Tayyar Energy is a private equity investor with several years experience working on high-risk energy investments in developing countries. Local investors are unwilling to take on the risks of such a novel project with an unproven technology. Hence, bioenergy project developers face more difficulty in getting finance. Without the subsidies, it is almost impossible to produce a bankable document for the loan proposal (Prasertsan, Sajjakulnukit 2005). In order to be incentivized to invest in the project with a technology unknown in Thailand, the foreign investors looked towards the added benefits from CDM⁷. The benefits from the CDM were an integral part of the investors' decision to proceed; benefits from CDM were considered with the other benefits from the project from the very start. Had carbon credits not been one of the benefits associated with the project, the investors would have been in a similar situation as local investors; they would have lacked the encouragement to invest. The benefits from carbon credits provide even further encouraged the investors to invest as revenue from carbon credits is in stable US dollars while all other revenues associated with the project activity are in the fluctuating Thai baht.

⁵ A study was conducted comparing the Net Present Value of alternative wastewater treatment systems. It was demonstrated that the NPV of anaerobic lagoons is 45% lower than that of aerobic systems (Arthur 1983). One of the key aspects about anaerobic ponds is that their main capital (land) is recoverable (Peña Varón 2003).

⁶ e.g. Another project by the same Project Developer replaced an old failed biogas reactor for this reason

⁷ Proof of this was provided to the validator.



In addition to the risk from the project activity, there was the very significant risk associated with the operation of the factory which produces the wastewater in the project activity. One example of this is, in 2005, there was a prolonged droughts that crushed cassava crop output (Partos 2005), harming the Thai cassava industry. Further demonstrated this risk is the fact that a number of cassava starch producing companies have experienced severe financial turmoil and bankruptcy⁸.

The commercial risks associated with anaerobic technology also apply to aerobic treatment systems as they are an unknown, risky and costly technology. There have high upfront costs associated and the O&M is costly and complicated due to the necessity of constant mechanical aeration (Parr, Smith and Shaw 2000). Additional costs are incurred by aerobic systems with the need for electricity for the aeration and removal of the production of large amounts of sludge.

Financial barriers are perceived to be major barriers to the project scenario of adopting AD technology and major barriers to the aerobic waste management alternative. Conversely, they do not pose barriers to the continued prevailing practice of pond systems.

Social

- Is this considered a well understood and accepted technology in the Host Nation and among local constituencies?

Are there Social barriers to alternative baseline practices?

- Current practice: This technology is an accepted technology, and continued operation of existing facilities presents no real social barriers. **No.**
- Anaerobic digestion: There is the risk of social perception being against a novel technology, however none have been observed in relation to this project, as a result of public engagement and the support of the facility management. **Yes.**
- Aerobic treatment: There is the risk of social perception being against novel technologies. **Yes.**

Where ponds are currently employed, few social barriers may be observed. They are accepted within the local environment and are the most popular operating practice in Thailand (FAO 2001). Anaerobic, and even aerobic facilities, present social barriers of perceived risk (explosion from biogas collection, smell etc), even where not merited, as the local community does not have knowledge of or experience with the anaerobic digestion technology. Although there still exists the potential for some perceived social risks, public engagement with regard to the Project activity have decreased this risk for the Project.

Social issues are therefore considered a minor barrier to the latter two scenarios and no barrier to the current pond based management system.

Business Culture

- Is there a willingness to change to alternative management practice in the absence of regulation?
- Is this technology considered 'standard practice' in the industry?

⁸ As demonstrated to the validator.



- Is there experience of applying the technologies?
- Is this technology considered a high management priority, as a result of its familiarity?

Are there business culture or other barriers to alternative baseline practices?

- Current practice: This technology is an accepted technology, and continued operation of existing facilities presents no real barriers. **No.**
- Anaerobic digestion: There is no experience of implementing such technologies in a Thai context and no strong drivers to become energy self-sufficient. **Yes.**
- Aerobic treatment: There is no experience of implementing such technologies in a Thai context. **Yes.**

As discussed in previous sections, the current pond based treatment is considered standard operating practise in Thailand and the region for wastewater treatment. The project activity, on the other hand, is not the standard operating practise. There is little experience of utilising aerobic or anaerobic technologies in a Thai context, and therefore these are not considered a high management priority. Additionally, there is a low level willingness to change from the current practice as it is efficient, low cost and in compliance with regulation.

The highest priority for most in the cassava sector is the management of waste discharges by simply maintaining compliance with local regulation at the lowest cost possible. Energy production, which is capital intensive and requires even greater management resources than the simple digestion process, is not a priority as electricity prices in Thailand are reasonable due to the government charging a uniform retail price throughout the country, with residential and industrial customers paying similar prices. Subsequently, this results in significant cross-subsidies between the industrial and residential sectors (World Energy Council 2001).

Business culture issues are therefore considered a barrier to the latter two scenarios and no barrier to the current pond based management system.

Step 4: Compare which is the most plausible baseline option:

The barriers analysis above has clearly shown that the most plausible baseline scenario is the prevailing practice of pond systems. In the situation where both anaerobic and aerobic wastewater treatment are considered, the most significant barriers are technology familiarity, perceived risks and the relative lack of investment interest among the key business constituency. The lack of experience with AD in the cassava industry in Thailand leaves most potential participants perceiving a very high risk.

In addition to the technical and social barriers of the Project activity, there are also associated financial barriers. As the Project activity is risky while the baseline scenario is safe, well known and inexpensive, there is little motivation to invest in the Project activity. This is demonstrated by the necessity of investment by foreign investors specializing in high risk projects.

Therefore, the context of the historical and future circumstances of the underlying asset, there are no barriers to current pond system wastewater treatment and significant financial and technical barriers to the alternatives, including Anaerobic Digestion.

**Timeline of events**

Event	Date
Contract signed with carbon advisor ⁹	09/12/2004
Start of project activity ¹⁰	01/03/2005
Approval of AM0022, version 1	13/05/2005
Start of validation ¹¹	29/10/2005
Start of commissioning ¹²	14/08/2006

Barriers Analysis Results Summary

Barrier Tested	Plausible Baseline Alternative	Direct Discharge to water bodies	Continuation of current practices	Anaerobic digestion	Aerobic treatment
Legal					
<ul style="list-style-type: none"> Does the practice violate any host country laws or regulations or is it not in compliance with them? 		Y	N	N	N
Technical					
<ul style="list-style-type: none"> Is this option currently difficult to purchase through local equipment suppliers? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Are skills and labour to operationalize and maintain this technology in country insufficient? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Is this technology outside common practice in similar industries in the country? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Is performance certainty not guaranteed within tolerance limits? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Is there real, or perceived, technology risk associated with the technology? 		N/A	N	Y	Y
Financial					
<ul style="list-style-type: none"> Is the technology intervention financially less attractive in comparison to other technologies (taking into account potential subsidies, soft loans or tax windows available)? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Is equity participation difficult to find locally? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Is equity participation difficult to find internationally? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Are site owners/project beneficiaries carrying any risk? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Is technology currency (country) denomination a risk? 		N/A	N	Y	Y
<ul style="list-style-type: none"> Is the proposed project exposed to commercial risk? 		N/A	N	Y	Y
Social					
<ul style="list-style-type: none"> Is the understanding of the technology low in the host country/industry considered? 		N/A	N	Y	Y
Business Culture					
<ul style="list-style-type: none"> Is there a reluctance to change to alternative management practices in the absence 		N/A	N	Y	Y

⁹ Contract between EcoSecurities and project developed has been shown to the DOE

¹⁰ Final budget was provided by the technology provider and so, decision to proceed with the project activity could be made. Evidence has been shown to the DOE.

¹¹ <http://cdm.unfccc.int/Projects/Validation/DB/RF2LZ8QUJWUXSVP896TRGY1A4KYR29/view.html>

¹² Proof of the start of commissioning has been shown to the DOE



regulation?				
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Step 5: Investment analysis

As specified in AM0022, this step is not necessary as there is only one baseline option result.

Step 6: Conclusion

The baseline determination demonstrates that the current and historic practices (and emissions), the use of the pond treatment, would continue in the absence of the CDM project activity. No other alternative baseline option is more likely therefore AM0022 is applicable.

B.5. Description of how the anthropogenic emissions of GHG by sources are reduced below those that would have occurred in the absence of the registered CDM project activity (assessment and demonstration of additionality): >>

As according to the additionality procedures in AM0022, version 04, given that the baseline determination in this project (see section B.4.) demonstrates that the baseline is different from the proposed project activity not undertaken as a CDM project activity, it is concluded that the project is additional.

B.6. Emission reductions:

B.6.1. Explanation of methodological choices:
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As per methodology AM0022, Version 4, emission reductions of the project activity are equal to baseline emission minus project emissions. Leakage is considered to be negligible.

Total Project emissions

Total estimated project emissions are the sum of fugitive methane emissions from the existing lagoon-based water treatment system, from possible methane emissions from the new anaerobic waste water treatment facility, from incomplete biogas combustion, biogas leaks.

$$E_{project} = E_{CH4_lagoons} + E_{CH4_NAWTF} + E_{CH4_IC+Leaks} \quad (1)$$

where:

- $E_{project}$ are the Total Project Emissions (tCO₂e)
- $E_{CH4_lagoons}$ are the fugitive methane emissions from lagoons from Equation (2) (tCO₂e)
- E_{CH4_NAWTF} are the fugitive methane emissions from the new anaerobic wastewater treatment facility (tCO₂e)
- $E_{CH4_IC+leaks}$ are the methane emissions from inefficient combustion and leaks (tCO₂e)



To calculate methane emissions from inefficient combustion and leaks, the “Tool to determine project emissions from flaring gases containing methane” was used for the flaring component. As the project activity utilises an open flare, the default flare efficiency – as stated by the tool – is 50%.

Total Baseline Emissions

Total estimated baseline emissions are the sum of fugitive methane emissions from the existing lagoon-based water treatment system and CO₂ emissions from the generation of heat on site (through the combustion of fuel oil) and the generation of power off site (from Thailand’s national electricity grid).

$$E_{BL} = E_{CH4_lagoons_BL} + E_{CO2_heat_BL} + E_{CO2_grid_BL} \quad (2)$$

where:

- **E_{BL}** are the Total Baseline Emissions (tCO₂e)
- **E_{CH4_lagoons_BL}** are the fugitive methane emissions from lagoons in the baseline case (tCO₂e). They are calculated with baseline data based on Equation (2) in the section on project emissions.
- **E_{CO2_heat_BL}** are the CO₂ emissions from on site fossil heat and/or power generation in the baseline case (tCO₂) that are displaced by generation based on biogas collected in the anaerobic treatment facility.
- **E_{CO2_grid_BL}** are the CO₂ emissions related to electricity supplied by the grid in the baseline case (tCO₂) that are displaced by generation based on biogas collected in the anaerobic treatment facility.

As stated above, baseline emissions include the CO₂ emissions from onsite heat generation and electricity from the grid.

As the gen sets of the Project have a capacity of less than 15 MW, AMS.I.D., version 12, of Appendix B of the SSC was used to determine an appropriate grid CEF. AMS.I.D. sets out two methods to develop such a CEF in grids not comprising fuel oil or diesel generation systems:

1. Average of build and operating margin where the operating margin excludes certain technology types).
2. Weighted average emissions of the generation mix.

In this situation, the combined margin was chosen and both the build margin and operating margin were calculated in keeping with AMS ID, version 12.

Total Emissions Reductions

$$ER = E_{BL} - E_{project} \quad (3)$$

Where:

ER: Emission reduction (t CO₂e)

E_{BL}: Baseline emissions (t CO₂e)



$E_{project}$: Project Emissions (t CO₂e)

It must be verified that the equation delivers a conservative estimate of emission reductions i.e. that the emissions of CH₄ from the lagoons in the baseline situation are not higher than the total emissions of biogas from the digester and the lagoons in the project situation.

B.6.2. Data and parameters that are available at validation:

(Copy this table for each data and parameter)

Data / Parameter:	EF _{CH₄}
Data unit:	kg CH ₄ /kg COD
Description:	Methane emission factor
Source of data used:	AM0022
Value applied:	0.21
Justification of the choice of data or description of measurement methods and procedures actually applied :	The 2006 IPCC default of 0.25 kg CH ₄ /kg COD has been corrected to 0.21 kg CH ₄ /kg COD to account for uncertainties. This is also the value applied in AM0022.
Any comment:	
Data / Parameter:	GWP _{CH₄}
Data unit:	
Description:	Global Warming Potential of methane
Source of data used:	AM0022
Value applied:	21
Justification of the choice of data or description of measurement methods and procedures actually applied :	IPCC default, as established in the Kyoto Protocol
Any comment:	
Data / Parameter:	M _{lagoon aerobic}
Data unit:	kg COD/ha/day
Description:	Amount of organic material degraded aerobically in the lagoon system
Source of data used:	AM0022
Value applied:	254
Justification of the choice of data or description of measurement methods and procedures actually applied :	As provided by the methodology and tested by the sensitivity analysis



Any comment:	
Data / Parameter:	R_{lagoon}
Data unit:	%
Description:	Total organic material removal ratio of the lagoon
Source of data used:	Project developer
Value applied:	98.2
Justification of the choice of data or description of measurement methods and procedures actually applied :	Determined in accordance with AM0022 prior to the start of the project activity through on-site biochemical testing in the lagoon system.
Any comment:	
Data / Parameter:	$R_{\text{deposition}}$
Data unit:	%
Description:	Organic material deposition ratio of the lagoon
Source of data used:	Project developer
Value applied:	2.1
Justification of the choice of data or description of measurement methods and procedures actually applied :	In accordance with AM0022, testing was done prior to the start of the project activity which determined the rate of deposition.
Any comment:	
Data / Parameter:	$NCV_{\text{fuel oil}}$
Data unit:	TJ/dm ³
Description:	Net calorific value of fuel oil
Source of data used:	IPCC 2006 and density from Engineer's Edge
Value applied:	39.996×10^{-6}
Justification of the choice of data or description of measurement methods and procedures actually applied :	IPCC default value from Table 1.2 of Chapter 1 of Vol.2 used for the NCV of fuel oil expressed in TJ/t. This value is multiplied by the density value of 0.99Kg/l from Engineer's Edge (http://www.engineersedge.com/fluid_flow/fluid_data.htm).
Any comment:	
Data / Parameter:	$EF_{\text{fuel oil}}$
Data unit:	tCO ₂ /TJ
Description:	Carbon emission factor of the fuel oil
Source of data used:	IPCC 2006
Value applied:	77.367
Justification of the	IPCC default value from Table 1.3 of Chapter 1 of Vol.2 gives an EF for



choice of data or description of measurement methods and procedures actually applied :	residual fuel oil of $21.1 \text{ kg}_{\text{carbon}}/\text{GJ}_{\text{fuel oil}}$. Applying the coefficient 44 g of CO ₂ /12 g of Carbon gives 77.367 tCO ₂ /TJ.
Any comment:	
Data / Parameter:	Grid CEF
Data unit:	tCO ₂ e/MWh
Description:	Carbon emission factor for the electricity displaced by the electricity generated from the biogas
Source of data used:	Electricity Generating Authority of Thailand (EGAT)
Value applied:	0.524
Justification of the choice of data or description of measurement methods and procedures actually applied :	The most recent available three years historical data from EGAT at the time of the start of validation was used to follow the methodological requirements set out in AMS.I.D. version 12, which follows the calculations of ACM0002, version 06
Any comment:	
Data / Parameter:	Lagoon surface area
Data unit:	hectare
Description:	Total lagoon area
Source of data used:	Project developer
Value applied:	1.105
Justification of the choice of data or description of measurement methods and procedures actually applied :	
Any comment:	
Data / Parameter:	Flare efficiency
Data unit:	%
Description:	Flare efficiency for open flare
Source of data used:	Tool to determine project emissions from flaring gases containing methane
Value applied:	50
Justification of the choice of data or description of measurement methods and procedures actually applied :	This is calculated according to the “Tool to determine project emissions from flaring gases containing methane” for open flares which consists of using a 50% default if a flame is detected for at least 20min in the hour and ensuring that flare is operated properly.
Any comment:	



Data / Parameter:	$R_{SO_4^{2-}}$
Data unit:	Kg/tonne (kg_{COD}/tSO_4^{2-})
Description:	Reduction factor for SO_4^{2-} oxidative substance
Source of data used:	AM0022 v4
Value applied:	651
Justification of the choice of data or description of measurement methods and procedures actually applied :	AM0022 v4 states in p.32 under the section <u>Determining losses of Chemical Oxygen Demand through chemical oxidation</u> : “where the concentration of sulphate is observed to be $1\text{ kg}/\text{m}^3$ of waste water, $0.651\text{ kg}/\text{m}^3$ of Chemical Oxygen Demand will be removed through chemical reaction with the sulphate” hence the reduction factor is $0.651\text{ kg}_{COD}/\text{kgSO}_4^{2-} \Rightarrow 651\text{ kg}_{COD}/tSO_4^{2-}$.
Any comment:	

B.6.3 Ex-ante calculation of emission reductions:

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As per the equation set out in AM 0022, the following equations are used to estimate project emissions.

Total Project Emissions

Total estimated project emissions are the sum of fugitive methane emissions from the existing lagoon-based water treatment system, from possible methane emissions, the new anaerobic wastewater treatment facility, incomplete biogas combustion, and biogas leaks

$$E_{project} = E_{CH_4_lagoons} + E_{CH_4_NAWTF} + E_{CH_4_IC+Leaks} \quad (1)$$

where:

- $E_{project}$ are the Total Project Emissions (tCO₂e)
- $E_{CH_4_lagoons}$ are the fugitive methane emissions from lagoons (tCO₂e)
- $E_{CH_4_NAWTF}$ are the fugitive methane emissions from the new anaerobic wastewater treatment facility (tCO₂e)
- $E_{CH_4_IC+leaks}$ are the methane emissions from inefficient combustion and leaks (tCO₂e)

Total Project Emissions (TCO₂e)



Year	E _{CH4_lagoons} (tCO2)	E _{CH4_NAWTF} (tCO2)	E _{CH4_IC+leaks} (tCO2)	E _{project} (tCO2)
2009	6,049	-	4,741	10,791
2010	6,049	-	4,741	10,791
2011	6,049	-	4,741	10,791
2012	6,049	-	4,741	10,791
2013	6,049	-	4,741	10,791
2014	6,049	-	4,741	10,791
2015	6,049	-	4,741	10,791
2016	6,049	-	4,741	10,791
2017	6,049	-	4,741	10,791
2018	6,049	-	4,741	10,791
Total	60,494	-	47,414	107,908
Average	6,049	-	4,741	10,791

Fugitive Methane Emissions from Lagoons

Fugitive Methane Emissions from Lagoons are:

$$E_{CH4_lagoons} = M_{lagoon_anaerobic} \cdot EF_{CH4} \cdot GWP_{CH4} / 1000 \quad (2)$$

where:

- **M_{lagoon_anaerobic}** is the amount of organic material removed by anaerobic processes in the lagoon system (kg COD)
- **EF_{CH4}** is the methane emission factor (kg CH₄ / kg COD). A default COD to Methane conversion factor of 0.21kg CH₄/kgCOD is used¹³.
- **GWP_{CH4}** is the Global Warming Potential of methane (GWP CH₄ = 21)

The total removal of COD from individual lagoons is a function of:

- Aerobic surface oxidation of COD;
- Chemical oxidation in lagoons (where oxidative species such as sulphate are present);
- Sedimentation of material that microbes are unable to degrade before they form a bottom sediment; and,
- COD degradation as a result of anaerobic micro bacterial activity.

The mass balance in the considered lagoon system provides the amount of organic material removed by anaerobic processes.

$$M_{lagoon_anaerobic} = M_{lagoon_total} - M_{lagoon_aerobic} - M_{lagoon_chemical_ox} - M_{lagoon_deposition} \quad (3)$$

where:

¹³ The IPCC Good Practice Guidance and Uncertainty Management in National Greenhouse Gas Inventories default of 0.25 kg CH₄/kg COD has been corrected to 0.21 kg CH₄/kg COD to account for uncertainties, as described in AM022.



- $M_{\text{lagoon_total}}$ is the total amount of organic material removed in the lagoon system (kg COD).
- $M_{\text{lagoon_aerobic}}$ is the amount of organic material degraded aerobically in the lagoon system (kg COD). Surface aerobic losses of organic material in pond-based systems equal to 254 kg COD per hectare of pond surface area and per day and is assumed to be lost through aerobic processes.
- $M_{\text{lagoon_chemical_ox}}$ is the amount of organic material lost through chemical oxidation in the lagoon system (kg COD).
- $M_{\text{lagoon_deposition}}$ is the amount of organic material lost through deposition in the lagoon system (kg COD).

COD Degraded Anaerobically in Lagoon System in Baseline Scenario

Year	$M_{\text{input_total}}$ (kgCOD)	$M_{\text{lagoon_input}}$ (kgCOD)	R_{lagoon}	$M_{\text{lagoon_total}}$ (kgCOD)	$M_{\text{lagoon_aerobic}}$ (kgCOD)	$M_{\text{lagoon_chemical_ox}}$ (kgCOD)	$M_{\text{lagoon_deposition}}$ (kgCOD)	$M_{\text{lagoon_anaerobic}}$ (kgCOD)
2009	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2010	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2011	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2012	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2013	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2014	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2015	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2016	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2017	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
2018	7,523,520	7,523,520	98%	7,388,849	95,428	217	150,470	7,142,734
Total	75,235,200	75,235,200	98%	73,888,490	954,278	2,173	1,354,234	71,427,335
Average	7,523,520	7,523,520	1	7,388,849	95,428	217	150,470	7,142,734

As prescribed by the methodology, a sensitivity analysis has been carried out to determine the suitability of the surface oxidation factor utilised in this project analysis. This is presented in Annex 5.

In order to assess the amount of COD actually entering the anaerobic system (the lagoons) the amount of COD removed as a result of the new wastewater treatment facility must be determined.

Project Organic Material Entering Lagoon System from New Anaerobic Water Treatment System is:

$$M_{\text{lagoon_input}} = M_{\text{input_total}} \cdot (1 - R_{\text{NAWTF}}) \quad (4)$$

where:

- $M_{\text{lagoon_input}}$ is the input of organic material from the new project anaerobic waste water treatment facility into the lagoon system (kg COD)
- $M_{\text{input_total}}$ is the total amount of organic material fed into the new project water treatment facility (kg COD)
- R_{NAWTF} is the total organic material removal efficiency of the new project water treatment facility (-). It is a project specific factor used to estimate how much COD will be removed from the system.

Total Material Removed In Lagoon System is:



$$M_{\text{lagoon_total}} = M_{\text{lagoon_input}} \cdot R_{\text{lagoon}} \quad (5)$$

where:

- $M_{\text{lagoon_total}}$ is the total amount of organic material removed in the lagoon system through various routes (kg COD)
- R_{lagoon} is the total organic material removal ratio of the lagoon. A project specific factor, and is equal to the proportion of organic material removed (through all routes) within the boundaries of the lagoon system under consideration. This factor has been determined by carrying out a series of biochemical tests prior to project implementation. This value has been determined to be 98% for this project.

Material Deposition In Lagoon System is:

$$M_{\text{lagoon_deposition}} = M_{\text{lagoon_input}} \cdot R_{\text{deposition}} \quad (6)$$

where:

- $R_{\text{deposition}}$ is the organic material deposition ratio of the lagoon. It is equal to the proportion of organic material physically sedimented in lagoons within the project boundaries. It is a project specific factor derived from pre-project analysis

COD Degraded Anaerobically in Lagoon System in Project Scenario

Year	$M_{\text{input_total}}$ (kgCOD)	R_{NANTE} (%)	$M_{\text{lagoon_input}}$ (kgCOD)	R_{lagoon}	$M_{\text{lagoon_total}}$ (kgCOD)	$M_{\text{lagoon_aerobic}}$ (kgCOD)	$M_{\text{lagoon_chemical_ox}}$ (kgCOD)	$M_{\text{lagoon_deposition}}$ (kgCOD)	$M_{\text{lagoon_anaerobic}}$ (kgCOD)
2009	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2010	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2011	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2012	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2013	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2014	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2015	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2016	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2017	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
2018	7,523,520	80%	1,525,018	98%	1,497,720	95,428	44	30,500	1,371,747
Total	75,235,200	80%	15,250,175	98%	14,977,197	954,278	444	305,004	13,717,471
Average	7,523,520		1,525,018	1	1,497,720	95,428	44	30,500	1,371,747

Methane emissions from new anaerobic waste water treatment facility

In accordance with AM0022, methane emissions from the CIGAR should be assessed and estimated based on measurements, technology supplier data and expert estimates. They may be disregarded if documented evidence for their insignificance is given.

Methane emissions from Inefficient Combustion Emissions

The combustion of biogas methane may give rise to significant methane emissions as a result of incomplete, or inefficient combustion. The three predominant potential routes for the destruction of methane are:

- Biogas flaring;



- Biogas use in heating systems;
- Biogas use for on-site electricity generation.

This methane should be quantified through Equation (7).

$$E_{CH_4_IC+Leaks} = \left(\sum_r V_r \cdot C_{CH_4_r} \cdot (1 - f_r) \cdot GWP_{CH_4} \right) + PE_{flare} \quad (7)$$

Where:

the sum is made over two routes r for methane destruction (heating and electricity generation);

V_r is the biogas combustion process volume in route r (Nm³)

C_{CH_4} is the methane concentration in biogas (tCH₄/Nm³) to be expressed on wet basis. It is the product of the methane concentration in the biogas in Nm³_{CH₄}/Nm³_{Biogas} multiplied by the methane density at normal conditions.

f_r is the proportion of biogas destroyed by combustion (-)

PE_{flare} are the project emissions from flaring of the residual gas stream (tCO₂e) calculated following the procedures described in the “*Tool to determine project emissions from flaring gases containing Methane*”. PE_{flare} can be calculated on an annual basis or for the required period of time using this tool.

$$E_{CH_4_IC_heat} = V_{heat} \cdot C_{CH_4_r} \cdot (1 - f_{heat}) \cdot GWP_{CH_4}$$

$$E_{CH_4_IC_heat} = 6,556 * 340days * 58.7\% * 0.0007168 * (1-88\%) * 21$$

$$E_{CH_4_IC_heat} = 2332 \text{ tCO}_2/\text{yr}$$

$$E_{CH_4_IC_elec} = V_{elec} \cdot C_{CH_4_r} \cdot (1 - f_{elec}) \cdot GWP_{CH_4}$$

$$E_{CH_4_IC_elec} = 910 * 340days * 58.7\% * 0.0007168 * (1-98\%) * 21$$

$$E_{CH_4_IC_elec} = 54.68 \text{ tCO}_2/\text{yr}$$

$$E_{CH_4_IC_flaring} = 2,089 \text{ tCO}_2/\text{yr}$$

In the project activity, biogas will be flared only during equipment maintenance periods at the project site or during times where biogas production exceeds the combined capacity of the electricity gen sets and the dual fuel burner. Such occasions will be rare, however, and flare use will in fact be sporadic. Project emissions from the flare will be calculated using the “*Tool to determine project emissions from flaring gases containing Methane*”. Since no continuous monitoring takes place, the default flare efficiency prescribed by the tool is utilized. The calculation steps for project emissions are as follows:

Step 1. Determination of the mass flow rate of the residual gas that is flared

This step calculates the residual gas mass flow rate in each hour h , based on the volumetric flow rate and the density of the residual gas. The density of the residual gas is determined based on the volumetric fraction of all components in the gas.



$$FM_{RG,h} = \rho_{RG,n,h} \times FV_{RG,h} \quad \text{(Flare: 1)}$$

Where:

$FM_{RG,h}$: Mass flow rate of the residual gas in hour h (kg/h)

$\rho_{RG,n,h}$: Density of the residual gas at normal conditions in hour h (kg/Nm³)

$FV_{RG,h}$: Volumetric flow rate of the residual gas in dry basis at normal conditions in the hour h (Nm³/h)

As stated in the “Tool to determine project emissions from flaring gases containing Methane”, a simplified approach may be taken, in which only the volumetric fraction of methane is measured and the difference to 100% is considered as nitrogen (N₂). Hence, step 2 is not applicable to the chosen methodological application of the tool and not included here for clarity purposes. As the methane combustion efficiency of the flare will not be continuously monitored as a default value for open flares will be used, steps 3-4 are also not applicable and will not be included.

Step 5: Determination of methane mass flow rate in the residual gas on a dry basis

The quantity of methane in the residual gas flowing into the flare is the product of the volumetric flow rate of the residual gas ($FV_{RG,h}$), the volumetric fraction of methane in the residual gas ($fv_{CH_4,RG,h}$) and the density of methane ($\rho_{CH_4,n,h}$) in the same reference conditions (normal conditions and dry or wet basis).

$$TM_{RG,h} = FV_{RG,h} \times fv_{CH_4,RG,h} \times \rho_{CH_4,n} \quad \text{(Flare: 13)}$$

Where:

$FV_{RG,h}$: Volumetric flow rate of the residual gas in dry basis at normal conditions in hour h (Nm³/h)

$fv_{CH_4,RG,h}$: Volumetric fraction of methane in the residual gas on dry basis in hour h

$\rho_{CH_4,n}$: Density of methane at normal conditions (kg/m³)

$$TM_{RG,h} = 58 \times 58.7 \times 0.7168$$

$$TM_{RG,h} = 24.377 \text{ kg/hr}$$

Step 6: Determination of the hourly flare efficiency

The determination of the hourly flare efficiency depends on the operation of flare and the type of flare used.

In case of open flares, the flare efficiency in the hour h ($\eta_{flare,h}$) is:

- 0% if the flame is not detected for more than 20 minutes during the hour h.
- 50%, if the flame is detected for more than 20 minutes during the hour h

Hence a 50% flare efficiency is assumed during normal operating conditions.

Step 7: Calculation of annual project emissions from flaring

Project emissions from flaring are calculated as the sum of emissions from each hour h , based on the methane flow rate in the residual gas ($TM_{RG,h}$) and the flare efficiency during each hour h ($\eta_{flare,h}$), as follows:



$$PE_{flare,y} = \sum_{h=1}^{8760} TM_{RG,h} \times (1 - \eta_{flare,h}) \times \frac{GWP_{CH4}}{1000} \quad \text{(Flare: 15)}$$

Where:

$TM_{RG,h}$: Mass flow rate of methane in the residual gas in the hour h

$\eta_{flare,h}$: Flare efficiency in hour h

GWP_{CH4} : Global Warming Potential of methane valid for the commitment period

$$PE_{flare,y} = 24.377 * (1 - 50\%) * (21/1000) * 8160^{14}$$

$$PE_{flare,u} (E_{CH4_IC_flaring}) = 2,089 \text{ t CO}_2/\text{yr}$$

Total emissions from inefficient combustion emissions

$$E_{CH4_IC+Leaks} = 2,332 + 54.68 + 2,089$$

$$E_{CH4_IC+Leaks} = 4,475 \text{ tCO}_2/\text{yr}$$

Methane Emissions from Leaks in Biogas System

Leaks in the biogas system include leaks from any anaerobic digester and leaks from the biogas pipeline delivery system. A conservative value of 1% was included in the ex-ante emissions reductions calculations.

Methane emissions from the CIGAR are expected to be zero in this project. Leaks will be monitored on a daily basis and the pipeline will be pressurized annually, as required by AM0022.

The baseline scenario for the project is based on what would have happened in the absence of the project activities. In that case, the baseline scenario will be continued:

- Use of the facultative pond system to receive wastewater from the current facility;
- Use of heavy fuel oil to produce heat to dry starch;
- Use of electricity from the Thai national grid system.

Total Baseline Emissions:

$$E_{BL} = E_{CH4_lagoons_BL} + E_{CO2_heat+power_BL} + E_{CO2_grid_BL} \quad \text{(8)}$$

where:

- E_{BL} are the Total Baseline Emissions (tCO₂e)
- $E_{CH4_lagoons_BL}$ are the fugitive methane emissions from lagoons in the baseline case (tCO₂e). They are calculated with baseline data in the section on project emissions.

¹⁴ The facility operates 8,160 hr/yr



- $E_{CO_2_heat+powers_BL}$ are the CO₂ emissions from on-site fossil heat and/or power generation in the baseline case (tCO₂) that are displaced by generation based on biogas collected in the anaerobic treatment facility.
- $E_{CO_2_grid_BL}$ are the CO₂ emissions related to electricity supplied by the grid in the baseline case (tCO₂) that are displaced by generation based on biogas collected in the anaerobic treatment facility.

Baseline emissions

Year	$E_{CH_4_lagoons_BL}$ (tCO ₂)	$E_{CO_2_onsiteheat_BL}$ (tCO ₂)	$E_{CO_2_grid_BL}$ (tCO ₂)	E_{BL} (tCO ₂)
2009	31,499	3,634	384	35,517
2010	31,499	3,634	384	35,517
2011	31,499	3,634	384	35,517
2012	31,499	3,634	384	35,517
2013	31,499	3,634	384	35,517
2014	31,499	3,634	384	35,517
2015	31,499	3,634	384	35,517
2016	31,499	3,634	384	35,517
2017	31,499	3,634	384	35,517
2018	31,499	3,634	384	35,517
Total	314,995	36,342	3,836	355,172
Average	31,499	3,634	384	35,517

On Site Heat Generation Emissions displaced by generation based on biogas collected in the anaerobic treatment facility

In calculating CO₂ emissions from on site heat displaced by biogas collected in the anaerobic treatment, the use of fossil fuels is considered:

$$E_{CO_2_heat} = F \cdot NCV \cdot EF \quad (9)$$

where:

- **F** is the corresponding amount of fossil fuel used for on-site heat (tonnes fuel oil). This is estimated as product of: 1) Average specific fuel consumption for the output of the facility and 2) the annual production.
- **NCV_{fuel oil}** is the net calorific value of the fossil fuel considered (TJ/unit). A default IPCC value for NCV is applied in the absence of a site-specific value. This is 0.0404 TJ/t divided by the density which gives 39.9×10^{-6} TJ/dm³.
- **EF_{fuel oil}** is the carbon emission factor of the fossil fuel considered (tCO₂/TJ). This is 77.37t CO₂/TJ for this project.

$$E_{CO_2heat} = 1,174,144 \text{ dm}^3 \text{ fuel oil/yr} * 77.37 \text{ tCO}_2/\text{TJ} * 39.996 \times 10^{-6} \text{ TJ/dm}^3_{\text{fuel}}$$

$$E_{CO_2heat} = 3,634 \text{ t CO}_2/\text{yr}$$

*On site and/or off site Grid Power Generation Emissions displaced by generation based on biogas collected in the anaerobic treatment facility*

Baseline Grid Power Generation Emissions displaced by renewable generation is based on biogas collected from the anaerobic treatment facility. In this project, only electricity displaced from the grid through this biogas generated power is considered. The underlying facility is grid connected, and does not have its own additional electricity generators. The carbon emission factor will be quantified according to AMS1D, Version 12 Renewable Energy Projects for a Grid as installed electrical capacity is expected to be well below 15MW. At least 2.1 MW will be installed.

Displaced electricity CO₂ emissions are determined through:

$$E_{CO_2_grid} = EL \cdot CEF \quad (10)$$

Where:

- **EL** is the amount of electricity displaced by the electricity generated from the biogas collected from the anaerobic treatment facility. This is estimated as the product of average specific electricity consumption, estimated using 3 years historical data and the annual production (MWh/yr)
- **CEF** is the carbon emission factor of the grid as discussed above (tCO₂e/MWh)

$$E_{CO_2_grid} = 2.153 * 340^{15} \text{ MWh/yr} * 0.524 \text{ tCO}_2/\text{MWh}^{16}$$

$$E_{CO_2_grid} = 384 \text{ tCO}_2/\text{yr}$$

Use of AMS I.D. to determine an appropriate grid CEF sets out two methods to develop such a CEF in grids not comprising fuel oil or diesel generation systems:

1. Average of build and operating margin where the operating margin excludes certain technology types).
2. Weighted average emissions of the generation mix.

In this situation, Option 1 was chosen and both the build margin and operating margin were calculated in keeping with AMS.I.D. version 12 as prescribed in the methodology ACM0002, version 06. Detailed spreadsheets can be found in Annex 3.

Operating Margin, Thailand

OM				
	2002	2003	2004	Average
	0.639	0.615	0.615	0.623

¹⁵ It is estimated that about 8% of the electricity used will be generated through biogas.

¹⁶ This is based on the most recent data available at the time of submission of the CDM-PDD to the DOE for validation, as required by the Tool to calculate the emission factor for an electricity system

**Thai Build Margin**

BM
2004
0.425

The data used is taken from the 2004 Thai Power Development Plan (EGAT, 2004), the most recently available data at the time of submitting for validation. For more information, please see Annex 3. A weighted grid average CEF for the Thai National Grid of **0.524tCO₂/MWh** is calculated. The project has two gensets of 1.05 MW installed.

Baseline Organic Material Entering Lagoon System from Starch Facility:

$$M_{lagoon_input_BL} = M_{input_total} \quad (11)$$

where:

- $M_{lagoon_input_BL}$ is the value used to specify the amount of organic material flowing into the lagoon system from the CIGAR in the project scenario equation (kg COD).
- M_{input_total} is the total amount of organic material fed into the baseline water treatment facility (kg COD). It is the same amount as fed into the project water treatment facility.

In the baseline, organic material (COD) from the facility enters directly into the pond system with no degradation of the wastewater before entering the lagoon system and all the organic material to be treated enters the lagoon system. The pond based fugitive methane emissions are quantified by determining;

- How much material enters the pond system;
- How much is lost through aerobic and oxidative processes;
- How much is lost through sedimentation in the pond system; and
- How much is removed through anaerobic processes.

Leakage

As stated in AM0022, leakage is considered to be negligible.

Emissions reductions

$$ER = E_{BL} - E_{project} \quad (12)$$

Where:

- ER:** Emission reduction (t CO₂e)
- E_{BL}:** Baseline emissions (t CO₂e)
- E_{project}:** Project Emissions (t CO₂e)

It must be verified this equation delivers a conservative estimate of emission reductions i.e. that the emissions of CH₄ from the lagoons in the baseline situation are not higher than the total emissions of biogas from the digester and the lagoons in the project situation. Therefore calculate:



$$E_{conservativeness} = E_{CH4_lagoons_BL} - (E_{CH4lagoon} + E_{CH4_navtf} + E_{CH4_coll}) \quad (13)$$

Where:

E_{CH4_coll} is the amount of methane expressed in (tCO₂e) contained in the biogas collected from the anaerobic treatment facility (i.e. the sum of the biogas sent to the heaters, the biogas sent to the gen sets and the biogas sent to the flare.)

In accordance with AM0022, as this number is negative, it will not be deducted from the results obtained from equation 12. Please see section B.6.4 for a summary of the project activity and baseline emissions and the total emissions reductions.

B.6.4 Summary of the ex-ante estimation of emission reductions:

Year	Estimation of Project Activity emissions (tonnes CO ₂ e)	Estimation of Baseline emissions (tonnes CO ₂ e)	Estimation of emission reductions (tonnes CO ₂ e)
2009	10,791	35,517	24,726
2010	10,791	35,517	24,726
2011	10,791	35,517	24,726
2012	10,791	35,517	24,726
2013	10,791	35,517	24,726
2014	10,791	35,517	24,726
2015	10,791	35,517	24,726
2016	10,791	35,517	24,726
2017	10,791	35,517	24,726
2018	10,791	35,517	24,726
Total	107,908	355,172	247,264
Average	10,791	35,517	24,726

B.7 Application of the monitoring methodology and description of the monitoring plan:

B.7.1 Data and parameters monitored:

Data / Parameter:	WW _{input}
Data unit:	m ³
Description:	Daily wastewater flows entering system boundary



Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	1,844
Description of measurement methods and procedures to be applied:	Will be measured continuously with a cumulative flow meter located at the incoming pipe to the CIGAR and reading recorded daily
QA/QC procedures to be applied:	Flow meters should be subject to a regular maintenance and testing regime to ensure accuracy.
Any comment:	
Data / Parameter:	
Data unit:	WW _{output} m ³
Description:	Daily wastewater flow leaving project treatment facility.
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	1,705
Description of measurement methods and procedures to be applied:	Will be measured continuously with a cumulative flow meter located at the pipe leaving the CIGAR and reading recorded daily.
QA/QC procedures to be applied:	Flow meters should be subject to a regular maintenance and testing regime to ensure accuracy.
Any comment:	
Data / Parameter:	
Data unit:	COD _{input} kg COD/ m ³
Description:	Wastewater organic material concentration entering the project boundary
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	12
Description of measurement methods and procedures to be applied:	Wastewater is sampled and analysed onsite at the facility's laboratory daily.



QA/QC procedures to be applied:	Weekly samples are sent to an accredited analytical laboratory for cross-checking with on-site data i.e. to assure accuracy.
Any comment:	
Data / Parameter:	
Data unit:	COD _{output}
Description:	kg COD/m ³
Source of data to be used:	Wastewater organic material concentration leaving the treatment facility.
Value of data applied for the purpose of calculating expected emission reductions in section B.5	Measured
Description of measurement methods and procedures to be applied:	2
QA/QC procedures to be applied:	Wastewater is sampled and analysed onsite at the facility's laboratory daily.
Any comment:	Weekly samples are sent to an accredited analytical laboratory for cross-checking with on-site data i.e. to assure accuracy.
Data / Parameter:	
Data unit:	EL
Description:	MWh
Source of data to be used:	Electricity generated from the biogas collected in the anaerobic treatment facility and consumed on site or sent to the grid
Value of data applied for the purpose of calculating expected emission reductions in section B.5	Measured
Description of measurement methods and procedures to be applied:	2.153
QA/QC procedures to be applied:	This is measured continuously with a power meter and the reading will be recorded daily.
Any comment:	Regular maintenance on GE Jenbacher's includes maintenance on the Project Logic Control (PLC). The meter is calibrated regularly and generation is cross checked against invoices.
Data / Parameter:	
Data unit:	V _{heat}
Description:	Nm ³
Source of data to be used:	Volume of biogas sent to facility heaters.
	Measured



Value of data applied for the purpose of calculating expected emission reductions in section B.5	6,556
Description of measurement methods and procedures to be applied:	Volume in Nm ³ will be measured continuously by a flowmeter and a reading recorded daily.
QA/QC procedures to be applied:	Biogas meters should be subject to a regular maintenance and testing regime to ensure accuracy.
Any comment:	
Data / Parameter:	
	V _{flare} (also FV _{RG,h})
Data unit:	Nm ³
Description:	Biogas sent to flare
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	1,392
Description of measurement methods and procedures to be applied:	Volume in Nm ³ will be measured continuously by a flowmeter and reading recorded hourly
QA/QC procedures to be applied:	Biogas meters should be subject to a regular maintenance and testing regime to ensure accuracy.
Any comment:	This parameter is equivalent to the variable FVRG,h (volumetric flow rate of the residual gas in dry basis at normal conditions) as described in the “Tool to determine project emissions from flaring gases containing methane”
Data / Parameter:	
	V _{elec}
Data unit:	Nm ³
Description:	Biogas sent to gen sets
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	910
Description of measurement methods and procedures to be applied:	Volume in Nm ³ will be measured continuously by a flowmeter and reading recorded daily.



QA/QC procedures to be applied:	Biogas meters should be subject to a regular maintenance and testing regime to ensure accuracy.
Any comment:	
Data / Parameter:	C_{CH_4} (also $FV_{CH_4,v}$)
Data unit:	% of Nm^3/Nm^3
Description:	Biogas methane concentration
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	58.7
Description of measurement methods and procedures to be applied:	Measured continuously and data recorded daily. In case of a device breakdown, a portable gas analyser is used and data will be recorded hourly for as long as biogas is being pumped up until the fixed spectrometer is repaired and fitted.
QA/QC procedures to be applied:	
Any comment:	Also referred as $f_{V_{CH_4,h}}$ (Volumetric fraction of component i in the biogas in the hour h, where $i = CH_4$) in the “Tool to determine project emissions from flaring gases containing methane”. Only CH_4 will be monitored, the remaining part will be considered as N_2 (simplified approach according to Tool). The monitored value will actually have to be multiplied by the CH_4 density of $0.0007168 t_{CH_4}/m^3_{CH_4}$ from ACM0001 at normal conditions to obtain the value of C_{CH_4} in tCH_4/Nm^3 .
Data / Parameter:	$CSO_4^{2-}_{in}$
Data unit:	Tonnes/ m^3
Description:	Amount of chemical oxidising agents entering system boundary.
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	0.181×10^{-3}
Description of measurement methods and procedures to be applied:	The wastewater contains SO_4^{2-} which is an oxidising substance. Its concentration in wastewater at the entrance of the treatment facility will be monitored. Samples are collected daily, mixed, and concentration measured weekly. For emission reduction calculations the most recent value from testing will be kept until a new test result is received from the lab.
QA/QC procedures to be applied:	
Any comment:	This is used for the calculation of the baseline emissions.



Data / Parameter:	$C_{SO_4^{2-} \text{ out}}$
Data unit:	Tonnes/m ³
Description:	Amount of chemical oxidising agents out of the digester.
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	0.037×10^{-3}
Description of measurement methods and procedures to be applied:	The wastewater contains SO_4^{2-} which is an oxidising substance. Its concentration in wastewater at the outlet of the digester will be monitored. Samples are collected daily, mixed, and concentration measured weekly. For emission reduction calculations the most recent value from testing will be kept until a new test result is received from the lab.
QA/QC procedures to be applied:	
Any comment:	This is used for the calculation of the project emissions.
Data / Parameter:	f_{elec}
Data unit:	%
Description:	Gen set combustion efficiency
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	98
Description of measurement methods and procedures to be applied:	Annually
QA/QC procedures to be applied:	Gen sets are maintained regularly by GE Jenbacher to ensure optimal performance.
Any comment:	
Data / Parameter:	f_{heat}
Data unit:	%
Description:	Heating system combustion efficiency
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected	88



emission reductions in section B.5	
Description of measurement methods and procedures to be applied:	Annually
QA/QC procedures to be applied:	Boiler is maintained regularly by Weishaupt in order to ensure optimal performance.
Any comment:	There will be 2 boilers used: Bertrams Konus ($f_{\text{heat}}=87$) and Wieslock ($f_{\text{heat}}=89.5$). The average of the two boilers will be considered as overall f_{heat}
Data / Parameter:	
Data unit:	$WW_{\text{bypassing}}$
Description:	m^3
Source of data to be used:	Flow of wastewater directly to the current water treatment system, and bypassing the new wastewater treatment facility
Value of data applied for the purpose of calculating expected emission reductions in section B.5	Measured
Description of measurement methods and procedures to be applied:	0
QA/QC procedures to be applied:	A flowmeter is used to measure the wastewater bypassing the project facility
Any comment:	Regular maintenance and calibration of the flow meter
Data / Parameter:	
Data unit:	Biogas loss from pipeline
Description:	%
Source of data to be used:	Loss of biogas from pipeline
Value of data applied for the purpose of calculating expected emission reductions in section B.5	Measured
Description of measurement methods and procedures to be applied:	1
Any comment:	Integrity of biogas pipeline for losses of biogas methane will be tested annually through pressurizing the system and establishing pressure drops through leakage.



QA/QC procedures to be applied:	
Any comment:	In order to be a conservative, a 1% loss of biogas is used in ex-ante calculations.
Data / Parameter:	M_{Removed}
Data unit:	t COD
Description:	Organic material removed from wastewater facility
Source of data to be used:	Calculated
Value of data applied for the purpose of calculating expected emission reductions in section B.5	-
Description of measurement methods and procedures to be applied:	This parameter will be calculated based on monitored parameters $\text{COD}_{\text{input}}$ and $\text{COD}_{\text{output}}$.
QA/QC procedures to be applied:	
Any comment:	
Data / Parameter:	$\text{NCV}_{\text{biogas}}$
Data unit:	J/Nm^3
Description:	Biogas calorific value
Source of data to be used:	Measured
Value of data applied for the purpose of calculating expected emission reductions in section B.5	25,870,000
Description of measurement methods and procedures to be applied:	Samples are taken annually and sent to an external laboratory.
QA/QC procedures to be applied:	
Any comment:	The value used for estimations is the result of the product of an estimated 65% of biogas methane content with the NCV of methane of 55.53 MJ/kg and the methane density of $0.7168 \text{ kg}/\text{Nm}^3$.
Data / Parameter:	PE_{flare}
Data unit:	tCO ₂
Description:	Project emissions from flaring of the residual gas stream.
Source of data used:	Calculated



Value applied:	2,089
Justification of the choice of data or description of measurement methods and procedures actually applied :	This will be calculated according to the “Tool to determine project emissions from flaring gases containing methane” for open flares which consists of using a 50% default if a flame is detected for 20min in the hour and ensuring that flare is operated properly.
QA/QC procedures to be applied:	
Any comment:	
Data / Parameter:	F
Data unit:	dm ³
Description:	Fossil fuel volume equivalent to generate the same amount of heat generated from the biogas collected in the anaerobic treatment facility
Source of data used:	Measured and calculated
Value applied:	3,454.26
Justification of the choice of data or description of measurement methods and procedures actually applied :	Calculated from the monitored V_{heat} multiplied by monitored NCV_{biogas} and divided by fixed parameter $NCV_{\text{fuel oil}}$
QA/QC procedures to be applied:	
Any comment:	

B.7.2 Description of the monitoring plan:

>>

This section details the steps taken to monitor on a regular basis the GHG emissions reductions from the project.

Prior to the start of the crediting period, the organisation of the monitoring team will be established. Clear roles and responsibilities will be assigned to all staff involved in the CDM project. The Project Developer will have a designated staff member who will be responsible for monitoring emissions reductions of the project activity. All staff involved in the collection of data and records will be coordinated by the staff member in charge of monitoring. In addition to this staff, qualified personnel will be designated to handle and operate equipment and machinery at the project site.

Monitoring procedures will be established prior to the start of the project. These procedures will detail the organisation, control and steps required for certain key monitoring system features. This will ensure that high quality data is obtained. Specifically, data and records will be checked prior to being stored and archived. Data from the project will be checked to identify possible errors or omissions.



All data required for verification and issuance will be kept for at least two years after the end of the crediting period or the last issuance of CERs of this project, whichever occurs later. Data will be archived electronically and data backup will be maintained. Paper data back up will also be available.

All equipment will be calibrated and maintained in accordance to the manufacturer's recommendations to ensure accuracy of measurements. Records of calibration and maintenance will be retained as part of the CDM monitoring system.

B.8 Date of completion of the application of the baseline study and monitoring methodology and the name of the responsible person(s)/entity(ies)

>>

The baseline study was concluded in August 2007 following approval of a relevant methodology, AM0022. The baseline study was conducted by Courtney Blodgett (Courtney@ecosecurities.com) and Chanitra Dokmali (Ning@ecosecurities.com) at EcoSecurities.

SECTION C. Duration of the project activity / crediting period

C.1 Duration of the project activity:

C.1.1. Starting date of the project activity:

>>

01/03/2005¹⁷

C.1.2. Expected operational lifetime of the project activity:

>>

25 years

C.2 Choice of the crediting period and related information:

C.2.1. Renewable crediting period

C.2.1.1. Starting date of the first crediting period:

>>

Not Applicable

C.2.1.2. Length of the first crediting period:

>>

Not Applicable

¹⁷ This is 6 weeks *before* the date of the invoice for milestone 2 from the technology provider. As stated in the invoice, at this time, the final budget was provided and the decision to proceed with the project was made.

**C.2.2. Fixed crediting period:****C.2.2.1. Starting date:**

>>

01/01/2009 or on the date of registration of the CDM project activity

C.2.2.2. Length:

>>

10 (ten) years

SECTION D. Environmental impacts

>>

D.1. Documentation on the analysis of the environmental impacts, including transboundary impacts:

>>

This project does not require an Environmental Impact Assessment (EIA) under Thai Law. The project has tight project boundaries, with immediate physical impacts focused within these boundaries. These include:

- Dramatic reduction in biogas production and fugitive emissions of biogas from current pond system;
- Improved water quality in these ponds;
- Improved biodiversity impacts within the pond system environs.

Outside these boundaries, impacts felt at a national level include:

- Reduced demand for fossil fuel intensive grid fed electricity;
- Reduced demand for oil products.

D.2. If environmental impacts are considered significant by the project participants or the host Party, please provide conclusions and all references to support documentation of an environmental impact assessment undertaken in accordance with the procedures as required by the host Party:

>>

The positive environmental impacts mentioned above are considered significant, but by their nature are improvements on the current situation, and therefore do not require ongoing monitoring and management.

No significant negative environmental impacts have been identified, apart from the development of the CIGAR, which requires the development of previously unused land. This impact is not considered significant under Thai law, and does not require an EIA. Apart from the utilisation of this scrub-land, no other impacts (e.g., on ground water) or other environmental emissions can be determined.

SECTION E. Stakeholders' comments

>>

**E.1. Brief description how comments by local stakeholders have been invited and compiled:**

>>

TBEC invited a number of stakeholders to attend the Public Forum including government officials, local officials, NGOs, members of academia and others. The Public Participation event was publicized via the following channels:

- 1) Direct invitations: invitation letters were sent directly to the ONEP, Kalasin Industrial Estate and Owners of the host company as well as one other cassava processing company;
- 2) Adverts in newspaper: adverts, in English and Thai, informing stakeholders about the Public Participation event were placed in one Thai newspaper, *Siang Phupan Newspaper*. The advert ran for 15 days;
- 3) Word of mouth: TBEC's team spread the word among the local community.

The stakeholder consultation meeting was held 7 May 2005 at the Rimpao Hotel in Kalasin. The consultation was attended by 19 people. Presentations were given about the project and TBEC and climate change and the Clean Development Mechanism. After the presentations, a question and answer session was held. Audience member asked questions about governmental involvement and other biogas projects in Thailand. All of the questions were satisfactorily answered.

E.2. Summary of the comments received:

>>

No comments were received.

E.3. Report on how due account was taken of any comments received:

>>

Not applicable, given that no comments were received.

**Annex 1****CONTACT INFORMATION ON PARTICIPANTS IN THE PROJECT ACTIVITY**

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Annex 2

INFORMATION REGARDING PUBLIC FUNDING

This project will not receive any public funding.



Thai National Grid Build Margin

Plant name	Plant type	Capacity MW	Generation MWh	Annual Generation GWh/yr	Plant Efficiency %	Fuel Consumption TJ/year	Carbon Content tC/TJ	Oxidation %	Emissions tCO ₂ /yr	CEF t CO ₂ /MWh
Lamtakhong	hydro	500	264,000	264					0	0.00
Huai Yamo	hydro	1	2,000	2					0	0.00
Eastern power & Electricity	CC natural gas	350	2,356,000	2,356.00	50%	16,963.20	15.30	100%	951,636	0.40
Glow IPP	CC natural gas	713	5,314,000	5,314.00	50%	38,260.80	15.30	100%	2,146,431	0.40
Ratchaburi CC	CC natural gas	1,945	14,291,000	14,291.00	50%	102,895.20	15.30	100%	5,772,421	0.40
Ratchaburi thermal	natural gas	756	8,137	8.14	32%	91.54	15.30	100%	5,135	0.63
Krabi Thermal	fuel oil	340	1,386,000	1,386.00	33%	15,120.00	21.10	100%	1,169,784	0.84
Total			23,621,137						10,045,407	0.425
Percent of grid			22.25%							

Thai National Grid Combined Margin

OM	2002	2003	2004	Average
	0.639	0.615	0.615	0.623
BM				
2004	0.425			
CM				
2002-2004	0.524			

The plant data is taken from the 2004 Thai Power Development Plan (EGAT, 2004) and fuel values are from 2006 IPCC guidelines. From this analysis a weighted grid average CEF for the Thai National Grid of 0.524t CO₂/MWh is observed.



Inputs				
Value	Data Unit	Data/Parameter	Description	Source
1,844	m ³ /day	Q	Daily wastewater volume	Historical data
340	day/year		Operating days per year	Developer
626,960	m ³ /year	Q		Historical data
12,000	mg COD / l	COD_{in}		Historical data
1.81E-04	t/m ³	Cso₄2⁻_{in}	Concentration of oxidative substance SO ₄ ²⁻ at the entrance of the ww treatment facility	Historical data
3.70E-05	t/m ³	Cso₄2⁻_{out}	Concentration of oxidative substance SO ₄ ²⁻ at the effluent of the digester	Historical data
651	kg COD/t	R_{SO₄2⁻}	Specific reduction factor for SO ₄ ²⁻ oxidative substance	AM0022 v4
7,523,520	kg COD	M_{input_total}	total amount of org material fed into the new project water treatment facility	Calculated by COD _{in} and amount of ww
1.105	ha	A_{lagoon_aerobic}	surface area of anaerobic lagoons within project boundary	Developer
79.7%	ratio	R_{NAWTF}	org material removal efficiency of the new project water treatment facility	Historical data
98.21%	ratio	R_{lagoon}	org material removal ratio of the lagoon	Based on COD testing of wastewater entering and leaving the baseline anaerobic lagoons
2%	ratio	R_{dep}	org material deposition ratio of the lagoon	
3,011,720	Nm3/yr	V_{total}	Total amount of biogas produced	Historical data
1%	%	biogas_{loss}	Loss from leaks in biogas system	Conservative assumption
2,981,603	Nm3/yr	V_{total}	Total amount of biogas produced adjusted for leakage loss	Historical data
473,280	Nm3/yr	V_{flare}	biogas combustion process volume sent to flare	Historical data
2,229,040	Nm3/yr	V_{boiler}	Biogas sent to boiler	Historical data
309,400	Nm3/yr	V_{genset}	Biogas sent to genset	Historical data
88.2%	%	efficiency_{boiler}	Combustion efficiency	Manufacturer
98.0%	%	efficiency_{genset}	Combustion efficiency	Manufacturer
-	tCO ₂ e	E_{CH₄_NAWTF}	fugitive emissions from new anaerobic ww treatment facility	Assumed to be 0
2,089	tCO ₂ e	PE_{flare}	PE from PE from flaring tool	Calculated as according to flare tool
58.00	m ³ /h	FV_{RG,h}	Flow rate of biogas sent to flare	Historical data
58.7%	Fraction	fv_(CH₄,h)	Volumetric fraction of CH ₄ in the biogas	Historical data
Open	Type of flare		Type of flare	Developer
50%	%	n_{flare,h}	Default flare efficiency	In accordance with the flare tool
8160	h	h/yr	Operating hours per year	Developer
1,860,000	dm ³		Maximum amount of fossil fuel displaced by the use of the biogas	Developer
63%	%		Percent to be replaced by biogas	Historical data
1,174,448	dm ³	F	Amount of fossil fuel to be displaced	Historical data
9,221	MWh		Maximum amount of electricity displaced by the use of biogas	Developer
7.939%			Percent to be replaced by biogas	Historical data
732.0	MWh	EL	Amount of electricity to be replaced	Historical data (2007 only)
0.524	tCO ₂ /MWh	CEF	carbon emission factor for the electricity	Calculated based on ACM0002
Fuel oil			Fuel type	Developer
3.126	tCO ₂ /t fuel	EF	emissions factor of the fossil fuel	2006 IPCC



Annex 4

MONITORING INFORMATION

Data generated by the monitoring of the parameters relevant for the CDM project activity will be collected on-site and after quality checks transferred to EcoSecurities, who will perform a further quality check and calculate emission reductions.

In addition to the information contained within the main text of the PDD, to ensure the successful operation of the project and the credibility and verifiability of the emission reductions achieved, the project must have a well-defined management and operational system. It is the obligation of the operator to put such a system in place. It must include the operational procedures and responsibilities associated with the monitoring activities and adequate record keeping. In order to meet this requirement, the project developer has implemented ISO 9001 on the site and is now certified.



Annex 5
SURFACE OXIDATION SENSITIVITY ANALYSIS

Surface Oxidation Factor Sensitivity Analysis

An assessment is carried out here to determine the suitability of the 254kg COD/ha/day surface removal factor.

Surface Oxidation Factor Sensitivity Analysis

Surface Oxidative Removal Rate	Error Factor Applied	Baseline Lagoon Emissions	Sensitivity	Project emissions	Sensitivity	Emissions Reductions Estimated	Sensitivity
kg/ha/day	%	T CO ₂ e	%	T CO ₂ e	%	T CO ₂ e	%
254	-	35,517	-	10,791	-	24,726	-
318	25%	35,411	0.30%	10,685	0.98%	24,726	0.00
381	50%	35,307	0.59%	10,580	1.95%	24,726	0.00
508	100%	35,096	1.18%	10,370	3.90%	24,726	0.00
1,270	400%	33,834	4.74%	9,107	15.60%	24,726	0.00

The purpose of the sensitivity factor is to demonstrate that the surface area oxidation factor does not have significant or measurable influence on the total project emission reductions. A surface area oxidation factor of 254 kgCOD/ha/day was chosen based on the literature, but the sensitivity analysis shows that a higher surface area oxidation factor would not have produced a significant change in the emission reductions. This analysis clearly shows that the emissions reductions calculated are independent of the surface oxidative removal of COD in this project, and thus the 254kg COD/ha/day removal factor is appropriate for this project.

The baseline and project emissions scenarios were calculated using 254 kgCOD/ha/day, as per AM0022. If, however, the surface area oxidation constant were to be increased, emissions reductions would not change significantly. Changes that do occur when applying a higher surface area oxidation constant affect both the baseline and the project emissions such that a decrease in emission reductions is seen in both the baseline and project emissions, but that the difference between the two - the total project emissions - is the same as the total calculated using 254 kgCOD/ha/day. The total emissions reductions when the surface area oxidation constant is increased 100% to 508 kgCOD/ha/day remains constant. In effect, total emissions reductions show 0% sensitivity to the value used for surface area oxidation.



Annex 6
Barrier analysis documentation

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5th November 2007

Khun Chanitra Dokmali
CDM Project Manager
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10330, Thailand

Dear Khun Chanitra Dokmali,

Biogas Plant Operations Training for Thai Biogas Staff

This letter is to confirm that our Mr Neramit Arunkhajornsak provided a detailed training course to staff from the Kitroonruang, Jiratpattana and Chow Khun Agro sites of Thai Biogas Energy Company Ltd on 14 November 2006.

Yours faithfully,
Waste Solutions Ltd

Martin Campbell-Board
Project Manager



Annex 7

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