BASF The Chemical Company

STEULER Anlagenbau GmbH & Co. KG

Battery limit conditions

Supply pressure (min) 0.12 MPa- absolute

Or at sufficient pressure to be conveyed through a length and diameter of pipeline agreed by the parties, and discharged in a stack of height and diameter to be agreed between LYPC, STEULER and BASF.
Note: the current stack is 350mm diameter and 35 m tall. Because of dilution with air in the abatement unit, the gas flow will be about 4-fold higher so a new and larger stack will probably be required.

Supply Temperature goal for heat recovery design 70 to 110 deg C

(The temperature of the product stream will depend on the extent of energy recovery that is chosen by LYPC for STEULER to provide in the FEEP, based on economics or other considerations. The actual temperature also depends on how LYPC chooses to run the energy recovery system. There may be times that LYPC will chose not to recover energy from the hot product stream, for example, during times that boiler feed water supply is unavailable, or during maintenance of the heat recovery system.)

Design pressure	HOLD	barG
Design temperature	-40 to 400 deg	°C

The product stream flowrate and composition will vary with the feed composition, but is typically expected to be as follows, depending on the composition and flow of the feed gas, the activity of the catalyst, and the temperature of operation.

2.4.2 Catalyst N_2O- Efficiency

Guarantee of the N_2O conversation:	>95%
Expected N_2O conversation:	approx. 99%

2.4.3 Steam Quality

Supply pressure (min)	0.55 MPa- absolute
Supply pressure (max)	0.70 MPa- absolute
Quality	saturated steam

2.5 Consumption of Utilities, Catalysts & Chemicals

2.5.1 Typical Consumption of Utilities