



Indicative simplified baseline and monitoring methodologies  
for selected small-scale CDM project activity categories

### TYPE III - OTHER PROJECT ACTIVITIES

Project participants shall take into account the general guidance to the methodologies, information on additionality, abbreviations and general guidance on leakage provided at <http://cdm.unfccc.int/methodologies/SSCmethodologies/approved.html>.

#### III.I. Avoidance of methane production in wastewater treatment through replacement of anaerobic lagoons systems by aerobic systems

##### Technology/measure

1. This project category methodology comprises technologies and measures that avoid the production of methane from biogenic organic matter in wastewaters being treated in anaerobic lagoons systems. Due to the project activity, the anaerobic lagoons systems<sup>1</sup> (without methane recovery) are substituted by aerobic biological systems<sup>2</sup>. The project activity does not recover or combust methane in wastewater treatment facilities (unlike AMS-III.H).
2. Measures are limited to those that result in emission reductions of less than or equal to 60 kt CO<sub>2</sub> equivalent annually.

##### Boundary

3. The project boundary is the physical, geographical sites where:
  - (a) The wastewater treatment would have taken place and the methane emission occurred in absence of the project activity;
  - (b) The wastewater treatment takes place in the project activity;
  - (c) The sludge is treated and disposed off in the baseline and project situation.

##### Baseline

[Please note: the structure of methodology has changed, baseline emissions appear first followed by project emissions.]

4. The baseline scenario is the situation where, in the absence of the project activity, degradable organic matter in wastewater is treated in anaerobic lagoons systems and methane is emitted to the atmosphere. Baseline emissions are:
  - (a) calculated as the amount of methane produced in the anaerobic baseline wastewater treatment system(s) that was is/are being replaced with the biological aerobic system(s) ( $BE_{ww,treatment,y}$ )

<sup>1</sup> As defined in 2006 IPCC Guidelines for National Greenhouse Gas inventories, Volume 5, Chapter 6, Wastewater treatment and discharge, table 6.3 and 6.8. Under this methodology Anaerobic lagoons are ponds deeper than 2 meters, without aeration, ambient temperature above 15<sup>0</sup>C, at least during part of the year, on a monthly average basis, and with a volumetric loading rate of Chemical Oxygen Demand above 0.1 kg COD.m<sup>-3</sup>.day<sup>-1</sup>.

<sup>2</sup> Systems using oxygen and microbial action to treat wastewaters.

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- (b) Methane emissions on account of inefficiencies in the baseline wastewater treatment systems and presence of degradable organic carbon in the treated wastewater discharged into river/lake/sea etc. ( $BE_{ww,discharge,y}$ ).
- (c) Methane produced in the baseline sludge treatment system(s) ( $BE_{s,treatment,y}$ ).
- (d) Methane emissions from anaerobic decay of the final sludge produced in the baseline situation. If the sludge is controlled combusted, disposed in a landfill with biogas recovery, or used for soil application in the baseline scenario, this term shall be neglected ( $BE_{s,final,y}$ ).

$$BE_y = BE_{ww,treatment,y} + BE_{ww,discharge,y} + BE_{s,treatment,y} + BE_{s,final,y} \quad (1)$$

Where:

$BE_y$	Baseline emissions in the year $y$ ( $tCO_2e$ )
$BE_{ww,treatment,y}$	Methane produced in the anaerobic baseline wastewater treatment system(s) that is/are being replaced with the biological aerobic system(s) ( $tCO_2e$ )
$BE_{ww,discharge,y}$	Methane emissions on account of inefficiencies in the baseline wastewater treatment systems and presence of degradable organic carbon in the treated wastewater discharged into river/lake/sea etc. ( $tCO_2e$ )
$BE_{s,treatment,y}$	Methane produced in the baseline sludge treatment system(s) ( $tCO_2e$ )
$BE_{s,final,y}$	Baseline methane emissions from anaerobic decay of the final sludge produced ( $tCO_2e$ )

5. In the determination of baseline emissions using formula 1), historical records of at least one year prior to the project implementation shall be used. This shall include COD removal efficiency of the wastewater treatment systems, amount of dry matter in sludge, power and electricity consumption per  $m^3$  of wastewater treated, amount of final sludge generated per tonne of COD treated and all other parameters required for determination of baseline emissions.

6. In case one year of historical data are not available, the parameters shall be determined by a measurement campaign in the baseline wastewater systems of at least 10 days. The measurements should be undertaken during a period that is representative for the typical operation conditions of the systems and ambient conditions of the site (temperature, etc). Average values from the measurement campaign shall be used and the result shall be multiplied by 0.89 to account for the uncertainty range (30% to 50%) associated with this approach as compared to one-year historical data.

7. The baseline emissions from the anaerobic wastewater treatment ~~lagoon~~ system(s) are estimated as follows using the procedure defined under category AMS III.H:

$$BE_{ww,treatment,y} = \sum_{i,m} (Q_{ww,m,y} * COD_{removed,i,m,y} * MCF_{anaerobic,i}) * B_o * UF_{BL} * GWP_{CH4} \quad (2)$$



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[Please note:  $UF_{BL}$  added to formula and possibility for multiple systems introduced, similar to the currently approved AMS-III.H.  $UF_{BL}$  and  $UF_{PJ}$  also added to other formulas.]

Where:

- $Q_{ww,ym,y}$  Volume of the wastewater treated during the months  $m$ , during year  $y$ , for the months with ambient average temperature above  $15^{\circ}\text{C}$  ( $\text{m}^3$ )
- $i$  Index for baseline wastewater treatment system
- $MCF_{\text{anaerobic, lagoon}}$  Methane correction factor for the anaerobic baseline wastewater treatment system  $i$  in anaerobic lagoons replaced by the project activity, value as per Table III.I.1. (MCF lower value of 0.8 as per table III.H.1 under AMS-III.H).
- $COD_{\text{removed},i,m,y}$  Chemical oxygen demand removed<sup>3</sup> by the anaerobic wastewater treatment system  $i$  in the baseline situation in the year  $y$  for the months  $m$  with ambient average temperature above  $15^{\circ}\text{C}$  ( $\text{tonnes}/\text{m}^3$ )
- $UF_{BL}$  Model correction factor to account for model uncertainties (0.94)<sup>4</sup>
- $B_0$  Methane producing capacity for the wastewater (IPCC default value for domestic wastewater of  $0.21 \text{ kg CH}_4/\text{kg.COD}$ )<sup>5</sup>
- $GWP_{\text{CH}_4}$  Global Warming Potential for  $\text{CH}_4$  (value of 21)

To determine  $COD_{\text{removed},i,m,y}$ : as the baseline treatment system(s) is different from the treatment system(s) in the project scenario, the monitored values of the COD inflow during crediting period will be used to calculate the baseline emissions ex-post. The COD removed by the baseline system(s) shall be based on the removal efficiency of the baseline systems estimated as per paragraphs 5 or 6.

8. The Methane Correction Factor (MCF) shall be determined based on the following table:

**Table III.I.1. IPCC default values<sup>6</sup> for Methane Correction Factor (MCF)**

Type of wastewater treatment and discharge pathway or system	MCF value
Discharge of wastewater to sea, river or lake	0.1
Aerobic treatment, well managed	0
Aerobic treatment, poorly managed or overloaded	0.3
Anaerobic digester for sludge without methane recovery	0.8
Anaerobic reactor without methane recovery	0.8

<sup>3</sup> Difference of inflow COD and the outflow COD.

<sup>4</sup> Reference: FCCC/SBSTA/2003/10/Add.2, page 25.

<sup>5</sup> The IPCC default value of  $0.25 \text{ kg CH}_4/\text{kg COD}$  was corrected to take into account the uncertainties. For domestic waste water, a COD based value of  $B_{0,ww}$  can be converted to  $BOD_5$  based value by dividing it by 2.4 i.e. a default value of  $0.504 \text{ kg CH}_4/\text{kg BOD}$  can be used.

<sup>6</sup> Default values from chapter 6 of volume 5. Waste in 2006 IPCC Guidelines for National Greenhouse Gas Inventories



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Type of wastewater treatment and discharge pathway or system	MCF value
Anaerobic shallow lagoon (depth less than 2 metres)	0.2
Anaerobic deep lagoon (depth more than 2 metres)	0.8
Septic system	0.5

9. Methane emissions from degradable organic carbon in treated wastewater discharged in e.g. a river, sea or lake are determined as follows:

$$BE_{ww,discharge,y} = Q_{ww,y} * GWP_{CH4} * B_o * UF_{BL} * COD_{ww,discharge,BL,y} * MCF_{ww,discharge,BL} \quad (3)$$

Where:

$Q_{ww,y}$	Volume of treated wastewater discharged in year $y$ (m <sup>3</sup> )
$UF_{BL}$	Model correction factor to account for model uncertainties (0.94) <sup>7</sup>
$COD_{ww,discharge,BL,y}$	Chemical oxygen demand of the treated wastewater discharged into sea, river or lake in the baseline situation in year $y$ (tonnes/m <sup>3</sup> ).
$MCF_{ww,discharge,BL}$	Methane correction factor based on the discharge pathway (e.g. into sea, river or lake) of the wastewater (fraction) (MCF value as per table III.I.1)

To determine  $COD_{ww,discharge,BL,y}$ : As the baseline treatment system(s) is different from the treatment system(s) in the project scenario, the monitored values of the COD inflow during crediting period will be used to calculate the baseline emissions ex-post. The outflow COD of the baseline systems will be estimated using the removal efficiency of the baseline treatment systems, estimated as per paragraphs 5 or 6.

10. Methane emissions from the baseline sludge treatment systems “j” are determined as follows:

$$BE_{s,treatment,y} = \sum_j S_{j,BL,y} * MCF_{s,treatment,j} * DOC_s * UF_{BL} * DOC_F * F * 16/12 * GWP_{CH4} \quad (4)$$

Where:

$S_{j,BL,y}$	Amount of dry matter in the sludge that would have been treated by the sludge treatment system $j$ in the baseline scenario (tonne).
$j$	Index for baseline sludge treatment system
$DOC_s$	Degradable organic content of the untreated sludge generated in the year $y$ (fraction, dry basis). It shall be estimated using default values of 0.5 for domestic sludge and 0.257 for industrial sludge <sup>8</sup> .

<sup>7</sup> Reference: FCCC/SBSTA/2003/10/Add.2, page 25.

<sup>8</sup> The IPCC default values of 0.05 for domestic sludge (wet basis, considering a default dry matter content of 10 percent) or 0.09 for industrial sludge (wet basis, assuming dry matter content of 35 percent), were corrected for dry basis.

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$MCF_{s,treatment,j}$  Methane correction factor for the baseline sludge treatment system  $j$  (MCF values as per III.I.1).

$UF_{BL}$  Model correction factor to account for model uncertainties (0.94)<sup>9</sup>

$DOC_F$  Fraction of DOC dissimilated to biogas (IPCC default value of 0.5)

$F$  Fraction of  $CH_4$  in biogas (IPCC default of 0.5)

In case sludge is composted, the following formula shall be applied:

$$BE_{s,treatment,y} = \sum_j S_{j,BL,y} * EF_{composting} * GWP_{CH_4} \quad (5)$$

Where:

$EF_{composting}$  Emission factor for composting of organic waste (t  $CH_4$ /ton waste treated). Emission factors can be based on facility/site-specific measurements, country specific values or IPCC default values (table 4.1, chapter 4, Volume 5, 2006 IPCC Guidelines for National Greenhouse Gas Inventories). IPCC default value is 0.01 t  $CH_4$ /t sludge treated on a dry weight basis.

11. Since the baseline wastewater treatment system is different from the treatment system in the project scenario, the sludge generation rate (amount of sludge generated per unit COD removed) in the baseline situation may differ significantly from the project situation. The amount of sludge generated in aerobic wastewater systems is generally larger than that in anaerobic systems, for the same COD removal efficiency. Therefore, the monitored values of the amount of sludge generated during the crediting period shall be used to estimate the amount of sludge generated in the baseline, as follows:

$$S_{j,BL,y} = S_{l,PJ,y} * \frac{SGR_{BL}}{SGR_{PJ}} \quad (6)$$

Where:

$S_{l,PJ,y}$  Amount of dry matter in the sludge treated by the sludge treatment system  $l$  in year  $y$  in the project scenario (tonne).

$SGR_{BL}$  Sludge generation ratio of the wastewater treatment plant in the baseline scenario (tonne of dry matter in sludge/tonne COD removed). This ratio will be measured ex-ante through representative measurement campaign, or using historical records of COD removal and sludge generation in the baseline treatment systems as per the guidance in paragraph 5 or 6.

<sup>9</sup> Reference: FCCC/SBSTA/2003/10/Add.2, page 25.

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**SGR<sub>PJ</sub>** Sludge generation ratio of the wastewater treatment plant in the project scenario (tonne of dry matter in sludge/tonne COD removed). Calculated using the monitored values of COD removal and sludge generation in the project scenario.

12. Methane emissions from anaerobic decay of the final sludge produced in the baseline situation are determined as follows:

$$BE_{s,final,y} = S_{final,BL,y} * DOC_s * UF_{BL} * MCF_{s,BL,final} * DOC_F * F * 16 / 12 * GWP_{CH4} \quad (7)$$

Where:

**S<sub>final,BL,y</sub>** Amount of dry matter in final sludge generated by the baseline wastewater treatment in the year y (tonnes). It will be estimated using the monitored amount of dry matter in final sludge generated by the project activity (S<sub>final,PJ,y</sub>) corrected for the sludge generation ratios of the project and baseline systems as per formula 6 above.

**MCF<sub>s,BL,final</sub>** Methane correction factor of the disposal site that receives the final sludge in the baseline situation, estimated as per the procedures described in AMS-III.G.

**UF<sub>BL</sub>** Model correction factor to account for model uncertainties (0.94)

**Project Activity Emissions**

13. Project activity emissions consists of:

- (i) CO<sub>2</sub> emissions related to the power and fossil fuel used by the project activity facilities (PE<sub>power,y</sub>). Emission factors for grid electricity or diesel fuel use shall be calculated as described in category I.D;
- (ii) Methane emissions during the treatment of the wastewater in biological aerobic wastewater treatment systems (PE<sub>ww,treatment,y</sub>);
- (iii) Methane emissions from degradable organic carbon in treated wastewater discharged in sea/river or lake (PE<sub>ww,discharge,y</sub>);
- (iv) Methane emissions from sludge treatment in the project activity (PE<sub>s,l,y</sub>);
- (v) Methane emissions from the decay of the final sludge generated by the aerobic systems project activity, if the sludge is disposed to decay anaerobically in a landfill without methane recovery (PE<sub>sludges,final,y</sub>).

$$PE_y = PE_{power,y} + PE_{ww,treatment,y} + PE_{ww,discharge,y} + PE_{s,treatment,y} + PE_{s,final,y} \quad (8)$$

Where:

**PE<sub>y</sub>** Project activity emissions in the year y (tCO<sub>2</sub>e)

**PE<sub>y,power,y</sub>** Emissions on account of electricity or diesel fossil fuel consumption in the year y (tCO<sub>2</sub>e)



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$PE_{y,ww,treatment,y}$	Methane Emissions from the biological aerobic wastewater treatment in the year $y$ (tCO <sub>2</sub> e)
$PE_{ww,discharge,y}$	Methane emissions on account of inefficiencies in the project wastewater treatment systems and presence of degradable organic carbon in the treated wastewater discharged into river/lake/sea etc. (tCO <sub>2</sub> e)
$PE_{y,sludge,final,y}$	Methane Emissions from anaerobic decay of the final sludge produced in the year $y$
$PE_{s,treatment,y}$	Methane produced in the project sludge treatment system(s) (tCO <sub>2</sub> e)

14. Project activity emissions from electricity and fossil fuel consumption ( $PE_{power,y}$ ) are determined as per the procedures described in AMS-I.D. The energy consumption of all equipment/devices installed by the project activity, *inter alia* all equipment to treat wastewater and sludge shall be included. For project activity emissions from fossil fuel consumption the emission factor for the fossil fuel shall be used (tCO<sub>2</sub>/tonne). Local values are to be used, if local values are difficult to obtain, IPCC default values may be used. If recovered methane is used to power auxiliary equipment of the project it should be taken into account accordingly, using zero as its emission factor.

15. Methane emissions during the biological aerobic treatment of wastewater are determined as follows ( $PE_{ww,treatment,y}$ ):

$$PE_{ww,treatment,y} = \sum_k (Q_{ww,k,y} * COD_{removed,k,y} * MCF_{aerobic,k}) * B_o * UF_{PJ} * GWP_{CH4} \quad (9)$$

Where:

$Q_{ww,k,y}$	Volume of the wastewater treated during the year $y$ (m <sup>3</sup> )
$k$	Index for project wastewater treatment system
$COD_{y,removed,k,y}$	Chemical oxygen demand of effluent entering removed by the aerobic system $k$ the lagoons in the year $y$ (tonnes/m <sup>3</sup> )
$MCF_{aerobic,k}$	Methane correction factor for the aerobic wastewater treatment in aerobic systems $k$ (MCF higher value value of 0.1 for well managed aerobic biological systems, or 0.4 for poorly managed or overloaded systems as per table III.H.1 in category III.H shall be taken)
$UF_{PJ}$	Model correction factor to account for model uncertainties (1.06) <sup>10</sup>

16. Methane emissions from degradable organic carbon in treated wastewater discharged in sea/river or lake in the project situation are determined as follows ( $PE_{ww,discharge,y}$ ):

<sup>10</sup> Reference: FCCC/SBSTA/2003/10/Add.2, page 25.

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$$PE_{ww,discharge,y} = Q_{ww,y} * GWP_{CH_4} * B_o * UF_{PJ} * COD_{ww,discharge,y} * MCF_{ww,discharge} \quad (10)$$

Where:

$Q_{ww,y}$	Volume of wastewater treated in the year $y$ (m <sup>3</sup> )
$COD_{ww,discharge,y}$	Chemical oxygen demand of the final treated wastewater discharged into sea, river or lake in the year $y$ (tonnes/m <sup>3</sup> )
$MCF_{ww,discharge}$	Methane correction factor based on discharge pathway of the wastewater (fraction) (MCF value in table III.I.1 for sea, river and lake discharge)
$UF_{PJ}$	Model correction factor to account for model uncertainties (1.06) <sup>11</sup>

17. Methane emissions from the project sludge treatment systems “I” are determined as follows:

$$PE_{s,treatment,y} = \sum_l S_{l,PJ,y} * MCF_{s,treatment,l} * DOC_s * UF_{PJ} * DOC_F * F * 16/12 * GWP_{CH_4} \quad (11)$$

Where:

$S_{l,PJ,y}$	Amount of dry matter in the sludge treated by the sludge treatment system $l$ in year $y$ (tonne).
$l$	Index for project sludge treatment system

In case sludge is composted, the following formula shall be applied:

$$PE_{s,treatment,y} = \sum_l S_{l,PJ,y} * EF_{composting} * GWP_{CH_4} \quad (12)$$

Where:

$EF_{composting}$	Emission factor for composting of organic waste (t CH <sub>4</sub> /ton waste treated). Emission factors can be based on facility/site-specific measurements, country specific values or IPCC default values (table 4.1, chapter 4, Volume 5, 2006 IPCC Guidelines for National Greenhouse Gas Inventories). IPCC default value is 0.01 t CH <sub>4</sub> /t sludge treated on a dry weight basis.
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18. In case of sludge is disposed on landfills without methane recovery, project emissions are determined as follows:

$$PE_{s,final,y,sludge} = S_{y,final,PJ,y} * DOC_{y,s} * MCF_s * UF_{PJ} * DOC_F * F * 16/12 * GWP_{CH_4} \quad (13)$$

<sup>11</sup> Reference: FCCC/SBSTA/2003/10/Add.2, page 25.





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Where:

$S_{y,final,PJ,y}$  Amount of dry matter in final sludge generated by the project wastewater treatment systems in the year  $y$  disposed on a landfill (tonnes).

$MCF_s$  Methane correction factor of the landfill that receives the final sludge, estimated as described in category AMS-III.G.

$UF_{PJ}$  Model correction factor to account for model uncertainties (1.06)<sup>12</sup>

If the sludge is controlled combusted, disposed in a landfill with methane recovery, or used for soil application, project emissions from sludge disposed ( $PE_{y,s,final,y}$ ) shall be neglected, and the end-use of the final sludge will be monitored during the crediting period.

### Leakage

19. If the aerobic treatment technology is equipment transferred from another activity or if the existing equipment is transferred to another activity, leakage effects at the site of the other activity are to be considered.

### Emission Reductions

#### Monitoring

20. The emission reduction achieved by the project activity will be measured-calculated as the difference between the baseline emission and the sum of the project emission and leakage.

$$ER_y = BE_y - (PE_y + LE_y) \quad (14)$$

Where:

$ER_y$  Emission reduction in the year  $y$  (tCO<sub>2</sub>e)

$LE_y$  Leakage emission in the year  $y$  (tCO<sub>2</sub>e)

#### Monitoring

21. Monitoring shall involve:

- (a) The amount of COD treated in the wastewater treatment plant(s) ( $COD_{in}$ ,  $COD_{out}$ ,  $COD_{ww,discharge,y}$ ,  $COD_{removed,k,y}$ ) shall be measured regularly in accordance to national or international standards. The amount of wastewater entering and/or exiting the project activity shall be monitored continuously and recorded to provide the total volume of wastewater treated flow ( $Q_{ww,y}$ ) shall be recorded.
- (b) The yearly amount of sludge produced and sludge generation ratio ( $S_{y,I,PJ,y}$ ,  $S_{y,final,PJ,y}$  and  $SGR_{PJ}$ ) shall be measured. In case of sludge extracted in a slurry

<sup>12</sup> Reference: FCCC/SBSTA/2003/10/Add.2, page 25.



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phase, the volume ( $m^3$ ) and dry matter content (tonnes/ $m^3$ ) shall be used to calculate  $S_{i,PI,y}$ . In case of sludge removal as solids,  $S_{i,PI,y}$  is measured by direct weighing and measuring its dry matter content through sampling, ~~directly measured by weight or indirectly by its volume and density. Its degradable organic content ( $DOC_{y,s}$ ) will be measured by representative sampling and analysis, in case the default value is not used.~~

(c) The amount of fossil fuel and electricity used by the project activity facilities;

22. In case a MCF value of zero is adopted for the project wastewater treatment system assuming that it is a well managed aerobic system, its operation shall be documented in a quality control program, monitoring the conditions and procedures that ensure the aerobic condition of the reactors, and that the operational parameters (e.g. running time of aerators, flows, COD loads) are kept within the limits of the engineering design parameters of the wastewater treatment system. In case the operational parameters are not within these limits for a period of time, a MCF value of 0.3 shall be taken for that period.

23. If the methane emissions from anaerobic decay of the final sludge were to be neglected because the sludge is controlled combusted, disposed in a landfill with methane recovery, or used for soil application, then the end-use of the final sludge will be monitored during the crediting period.

24. If the baseline emissions included the anaerobic decay of final sludge generated by the baseline treatment systems in a landfill without methane recovery, the baseline disposal site shall be clearly defined, and verified by the DOE.

**Project activity under a programme of activities**

The following conditions apply for use of this methodology in a project activity under a programme of activities:

25. In case the project activity involves the replacement of equipment, and the leakage effect of the use of the replaced equipment in another activity is neglected, because the replaced equipment is scrapped, an independent monitoring of scrapping of replaced equipment needs to be implemented. The monitoring should include a check if the number of project activity equipment distributed by the project and the number of scrapped equipment correspond with each other. For this purpose scrapped equipment should be stored until such correspondence has been checked. The scrapping of replaced equipment should be documented and independently verified.

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History of the document

Version	Date	Nature of revision
07	EB 42, Annex 18 26 September 2008	Include additional guidance on baseline determination and project emission calculations; The methodology restructured, provisions related to methane correction factor and related uncertainties have been revised.
06	EB 33, Annex 36 27 July 2007	Additional leakage guidance to allow for application under a programme of activities (PoA).
05	EB 31, Annex 23 04 May 2007	Clarifies how the number of months with average lagoon temperature above 15°C in AMS III.I is to be determined. Scope 15 excluded.
04	EB 28, Annex 27 15 December 2006	Revised AMS III.I, analogous to AMS III.H, based on 2006 IPCC Guidelines for National Greenhouse Gas Inventories. Expand applicability to activities in geographic locations where lagoon temperature is above 15°C for only a part of the year.
03	EB 25, Annex 27 21 July 2006	Clarify the applicability condition relating to residence time of wastewater being treated.
02	EB 24, 10 May 2006, paragraph 64 of the report	The Board at its twenty-fourth meeting noted that type III project activities might be able to achieve significant emission reductions, without exceeding the direct emissions limits i.e. 15 kilo tonnes CO <sub>2</sub> e applicable at the time. As an interim solution, the Board agreed to include the following text in all Type III categories: "This category is applicable for project activities resulting in annual emission reductions lower than 25,000 tonnes CO <sub>2</sub> e. If the emission reduction of a project activity exceeds the reference value of 25,000 tonnes CO <sub>2</sub> e in any year of the crediting period, the annual emission reduction for that particular year is capped at 25,000 tonnes CO <sub>2</sub> e."
01	EB 23, Annex 24 24 February 2006	Initial adoption.